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A modeling and simulation framework for electrokinetic nanoparticle treatment

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**A MODELING AND SIMULATION FRAMEWORK
FOR ELECTROKINETIC NANOPARTICLE
TREATMENT**

by

James Phillips, B S , M S

**A Dissertation Presented in Partial Fulfillment
of the Requirements for the Degree
Doctor of Philosophy**

**COLLEGE OF ENGINEERING AND SCIENCE
LOUISIANA TECH UNIVERSITY**

May 2011

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We hereby recommend that the dissertation prepared under our supervision
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A Modeling and Simulation Framework for Electrokinetic Nanoparticle Treatment

be accepted in partial fulfillment of the requirements for the Degree of
Doctor of Philosophy in Computational Analysis and Modeling

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ABSTRACT

The focus of this research is to model and provide a simulation framework for the packing of differently sized spheres within a hard boundary. The novel contributions of this dissertation are the cylinders of influence (COI) method and sectoring method implementations. The impetus for this research stems from modeling electrokinetic nanoparticle (EN) treatment, which packs concrete pores with differently sized nanoparticles. We show an improved speed of the simulation compared to previously published results of EN treatment simulation while obtaining similar porosity reduction results. We mainly focused on readily, commercially available particle sizes of 2 nm and 20 nm particles, but have the capability to model other sizes. Our simulation has graphical capabilities and can provide additional data unobtainable from physical experimentation.

The data collected has a median of 0.5750 and a mean of 0.5504. The standard error is 0.0054 at $\alpha = 0.05$ for a 95% confidence interval of 0.5504 ± 0.0054 . The simulation has produced maximum packing densities of 65% and minimum packing densities of 34%. Simulation data are analyzed using linear regression via the R statistical language to obtain two equations one that describes porosity reduction based on all cylinder and particle characteristics, and another that focuses on describing porosity reduction based on cylinder diameter for 2 and 20 nm particles into pores of 100 nm height.

Simulation results are similar to most physical results obtained from MIP and WLR. Some MIP results do not fall within the simulation limits, however, this is expected as MIP has been documented to be an inaccurate measure of pore distribution and porosity of concrete. Despite the disagreement between WLR and MIP, there is a trend that porosity reduction is higher two inches from the rebar as compared to the rebar-concrete interface. The simulation also detects a higher porosity reduction further from the rebar. This may be due to particles aggregating before reaching the rebar that can easily be seen in the graphical representation of the simulation cylinders.

The dissertation author has created a web based framework to allow an interdisciplinary team to work in concert with access to the simulation and the results generated. The results are stored into a MySQL database. The database currently holds 271 simulation runs. Simulation requests can be entered into a web interface and will automatically be processed in the order entered and the results stored into the database. Results can also be retrieved from the database and filtered based on any simulation parameter. Statistical analysis can be completed on the data points stored in the database by using version of Rweb modified by the dissertation author. The result is a collaborative framework that can be extended to address future investigations into pore packing and chloride blocking.

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PREFACE

The purpose of this work is significantly different from the work I completed on the Watson Project for the Louisiana Tech University under Mike O’Neal. I learned about many elements of working on a large program in concert with many collaborators while developing the JavaScript lab used in Watson Lab. The lab is still in use in Louisiana Tech University computer science classes today and is freely available at <http://watson.latech.edu/> [1]. It has also been used in Health Informatics and Information Management classes.

Through teaching Computer Science courses at Louisiana Tech University over a four year period, I have honed my skills at creating effective and efficient programs using meaningful techniques. A focus on programming and data structures has served me well in completing this simulation of electrokinetic nanoparticle (EN) treatment.

Computer scientists are often involved in projects that do not fall directly under the field of computer science. This is certainly the case in this EN simulation research as it requires the need for a strong background in engineering, chemistry and mathematics. It is unlikely for any one person to have all the expertise necessary to complete a simulation of this nature. For example, it certainly would be unreasonable to ask a computer scientist to create the design for a bridge, in the same way as it would be to ask an engineer to develop commercial software without assistance. It is our goal to create a

framework that can easily be used and understood by collaborators without a deep understanding of the programming principles that make it possible

In today's world, it is important to collaborate with many experts in various fields to solve complex problems. The impetus for this research was to create a program to demonstrate the electrokinetic nanoparticle (EN) treatment process in real time. For the purpose of this paper all terms related to the EN process will be identical to those used in [2]

The results of the simulation of the EN treatment of concrete and corresponding model were published at the 2008 World Multi-National Conference on Systemics, Cybernetics and Informatics [3]. The presentation was solely provided by the dissertation author and received the "Session's Best Paper Award." Simulation results were also presented informally to representatives from Entergy Nuclear, Mississippi, who provided financial support for the research from January 1, 2008 to December 31, 2008. The target application was to reinforce the walls of nuclear plants so they would not have to be replaced. Improvements to the simulation work continued after these presentations and the results are presented in this dissertation.

CHAPTER 1

INTRODUCTION

In this dissertation, we present a simulation and model using computational analysis techniques obtained from a background in computer science and mathematics. In this research, we use our model to describe the electrokinetic nanoparticle (EN) treatment for pores in concrete and run EN treatment simulations several hundred times. The simulation provides a low-cost alternative to performing EN treatments and provides a level of detail for individual pores that is unobtainable in physical experimentation. It has also been suggested that the simulation should be utilized in modeling the effect of nanoparticle treatments on human bones and teeth to treat a variety of medical conditions [4]. These health treatments are beyond the scope of this dissertation. This model and simulation will be useful in any scenario where there are many mobile particles that must flow from one area to another while respecting hard boundaries.

In this chapter, we briefly cover the objective, research tools, methodology, and main results. We also present an overview of this dissertation at the end of this chapter.

1.1 Objective

Our objective is to create a model and simulation that can be used to describe the electrokinetic nanoparticle (EN) treatment. EN treatment is a technique that shows promise for increasing the longevity of concrete. At the risk of gross oversimplification,

EN treatment can be considered as the packing of spherical nanoparticles of various size into concrete pores

A functional requirement of our simulation was that all particles must flow to their packed locations as opposed to being immediately placed there. It is desired that the simulation posses the capability to display the packing of pores in real time. Furthermore, we require that the simulation run in a reasonable amount of time and memory, while maintaining accurate results. We will show that our methods require significantly less time than previously published work on the EN treatment simulation presented at WMSCI while maintaining similar porosity reduction results.

We will determine how spheres pack under cylindrical boundary conditions by collecting and analyzing simulation data. We chose to represent the pore as a cylinder as it is the commonly assumed pore shape and also simplifies the problem [5]. The research will be considered successful if the results of an electrokinetic nanoparticle (EN) treatment can be predicted. An equation to predict the results based on input data such as the sphere sizes, ratios and cylinder heights and diameters is preferred. We have obtained two such equations which are presented in Section 1.4 with more details in Chapter 4.

1.2 Research Tools

Prototype versions of the simulation were coded in Sun Java and Microsoft Visual Studios C++. The current version is compiled with gcc in Linux and MingW in Windows in order to provide multi-platform support. A MySQL database is used to store results and simulation requests. An Apache web server serves a website with PHP server side code to access the MySQL database. Linux BASH scripts are used to interface the simulation code with the MySQL database. For statistical analysis, the R programming

language was utilized [6] Rweb is utilized as a web interface to the R language. Toodled was also embedded in the website to manage deadlines and goals for the research.

1.3 Methodology

Our particular research is intended to simulate the electrokinetic nanoparticle (EN) treatment on concrete in detail for individual pores. In our simulation, we model pores as cylinders and nanoparticles as spheres. We focus on nanoparticles of diameters 2 and 20 nanometers (nm). Spheres will be randomly introduced into the cylinder at a constant rate. Because concrete pores vary in height and diameter, we need to generate results for a range of cylinders with varying radii and heights.

As part of this research, two algorithms have been developed to improve the speed at which the EN treatment can be simulated. Cylinders of Influence (COI) and Sectoring. Both of these algorithms share additional optimizations compared to work previously presented by the author at the World Multi-Conference on Systemics, Cybernetics and Informatics (WMSCI) in 2008 [3]. Our algorithms simulate the flow of spheres from one end of a cylinder to the other while respecting the boundaries of the cylinder and all spheres. The simulation programs utilized for this research require no manual interaction once they have been started. Each simulation will automatically introduce spheres and will also detect when no more spheres can be packed into the cylinder. Simulation results are stored in a database created and managed with the MySQL database management system (DBMS).

COI utilizes a custom data structure to reduce the time requirements of moving each particle during the simulation. The custom data structure consisted of a collection of

priority queues built on linked lists. Each queue contained only one size of sphere, and iterators will keep tract of multiple points of interest in the structure. This method takes advantage of the assumption that spheres do not move far in the linked list structure when they are moved. This approach was developed under the assumption that cylinder diameter is relatively small compared to cylinder length. As a result, this approach limits the impact of cylinder height increases on the time required to move an individual particle. Changes to cylinder height generally have no effect on the time required to move an individual particle. Larger simulation height does allow more particles to be packed which requires more simulation time, but this is unavoidable in our model. The weakness of the COI method lies in diameter increases, and short cylinders with large diameter sizes quickly degenerate to the brute force method [7].

The sectoring method, formally known as a hierarchical grid method, was developed to simulate packing when cylinders were not limited by diameter [8]. The sectoring method uses more memory, but reduces the number of calculations required to move a particle to a constant unaffected by cylinder height and diameter. This method involves overlaying a three-dimensional grid over the cylinder. We refer to each indexable area of the grid as a sector. When a particle is moved it need only check nearby sectors, thus moving of individual particles can be done in a constant amount of time. Sector sizes are automatically chosen by the simulation based off of the sizes of spheres to be packed.

To validate the simulation, simulation runs were compared to live data and data from literature using statistical techniques. Multivariate statistical techniques were used to analyze the data from numerous simulation runs over a wide variety of parameters [9].

Regression analyses were conducted to create equations that can be used to characterize porosity reduction and predict future results

1.4 Main Results

The main results presented in this dissertation include two equations obtained from linear regressions and discussed in detail in Section 4.2. Equations 1 and 2 give porosity reduction (PR) of a packed cylinder given the characteristics of the cylinder and spheres with which it is packed. The cylinder has height C_H and diameter C_D both given in nanometers (nm). Particles have diameter S_D in nm. As we have multiple sizes of particles, we simply add a numerical subscript to denote differently sized particles. In this case, the larger size of particle is S_1 and the smaller size is S_2 . An analysis was completed only on cylinders of height 100 packed with spheres of 2 and 20 nm to obtain Equation 1

$$PR = 0.4757 - 0.00003 C_D + 0.0207 \ln(C_D) \quad (1)$$

Equation 1 is statistically significant, but only explains 59 percent of the variance. It does indicate that C_D has a better fit using a log transform. Performing a linear regression analysis in R on all results obtained from the simulation we obtain Equation 2 where PR is the porosity reduction

$$PR = 4441 + 0.0081 \ln(C_D) - 0.0003 C_H + 0.0066 S_{1D} - 0.0048 S_{2D} \quad (2)$$

Equation 2 is statistically significant and explains 0.86 percent of the variance. For this paper, the coefficients have been rounded to at most 5 decimal places, but the software is capable of 15 decimal point precision.

1.5 Overview

Specific information on concrete and other background necessary to understand the issues involved are contained in Chapter 2. Chapter 3 contains a detailed explanation of the model and methodology used to simulate the EN treatment process. This includes pseudocodes for the “brute force”, “cylinder of influence (COI)” and “sectoring” methods. The fixing of spheres as described in Section 3.5.2 reduces the number of calculations required significantly. The COI method is described in detail in Section 3.6.2. Specific details of the sectoring method can be found in Section 3.6.3. Chapter 4 contains the results and analyses of the simulation work including the two regression equations obtained. Analyses were completed using the R statistical language. Multiple linear regression was the primary statistical method utilized. Chapter 5 summarizes the results and gives an overview of future research directions.

CHAPTER 2

BACKGROUND

This chapter explains the background and motivation for this dissertation, including information on concrete and the electrokinetic nanoparticle (EN) treatment. The main motivating factor for this research stems from the ingress of chloride ions into the concrete. The chloride ions ultimately damage the concrete, which leads to the need for expensive repair or replacement. In 2001, the "Annual direct cost of highway and bridge repairs (largely related to reinforcement corrosion) was \$8.3 billion in the US Alone" [10]. Porosity reduction is the main deterrent used to combat the ingress of chloride ions. To understand the mechanism and solution of concrete damage, we must discuss the nature of concrete, mechanisms of concrete deterioration and the common solutions to combat deterioration. Given this information, we then describe the techniques of electrochemical chloride extraction (ECE) and electrokinetic nanoparticle (EN) treatment. We will also discuss the methods used to evaluate the porosity of concrete weight loss ratio (WLR) and mercury intrusion porosimetry (MIP).

2.1 Issues

In order to understand the impetus and methods for this research we will give information on the nature of concrete, properties of concrete, deterioration of concrete, and the importance of packing density of concrete.

2.1.1 Concrete

Concrete is composed of 12% cement. The function of cement in concrete is to bind aggregates and sand together in a solid mass [11]. A common type of cement is Portland cement. Components of Portland cement include tricalcium silicate (C3S), dicalcium silicate (C2S), tricalcium aluminate (C3A), and calcium aluminoferite (C4AF) [12]. Modest variations in proportions of ingredients in cement can have a huge impact on the final product [11]. The first step in the process of making cement is mixing the ingredients together and grinding them down into a fine powder referred to as clinker. The size of the particles of cement clinker range from 5 to 50 µm, and the shape is spherical. Cement paste is formed by mixing cement clinker with water. The cement paste then hardens to form cement [12].

2.1.2 Properties of Concrete

The physical effects of chloride ingress and increased porosity of concrete are evident in the performance properties of concrete. Properties of concrete which affect the performance of concrete include shrinkage, elasticity, strength and creep [13]. Shrinkage refers to the decrease in volume of concrete during an extended time period which occurs due to changes in physio-chemical properties and moisture [14].

The shear resistance of concrete is affected by compressive strength, the ratio of shear span to depth and the ratio of embedded steel to concrete [15]. Compressive strength refers to the amount of pressure concrete can withstand without breaking. Greater levels of compressive strength in concrete positively correlate with tensile strength and negatively correlate with elasticity and creep [16].

Porosity is an intrinsic characteristic of cement mortar, concrete, and cement paste. Pores allow for liquid and gas penetration. Pores can be found in a variety of shapes with cylindrical pores being “the most commonly assumed shape”. Performance properties of concrete are affected by pore structure. Pore structure refers to pore size, pore connectivity, pore shape, total pore volume, pore distribution, surface area of pores, and number of pores [5]. Increased porosity increases chloride permeability into concrete, which negatively impacts performance properties of concrete [13].

Types of pores include capillary pores, gel pores, air voids, and hollow-shell pores. Gel pores tend to be the smallest pores, being only a few nanometers. Gel pores are formed from C-S-H gel, which is the primary binder ingredient that gives microstructure and strength to cement paste. Capillary pores are channels of interconnected pores, ranging from 2 nm to 10 μm in size. Not all of the water added to the cement is used in the chemical reactions that occur during the hardening of concrete. The capillary pores form due to this “capillary water”. Hollow-shell pores are the shape of a cement grain and range from 1 to 15 μm . Hollow-shell pores form when a cement grain does not hydrate and the cement grain recedes, creating a hollow-shell pore. Hollow-shell pores are difficult to identify using the mercury intrusion porosity, which is an often used technique for characterizing pore structures. Air voids form due to air becoming trapped during formation of concrete. Air voids may be several millimeters in size, but do not affect permeability of concrete structures [5].

2.1.3 Deterioration

Concrete structures may need to have a service life of a few years or a few centuries [17]. Decreased durability and service life of concrete structures is often caused

by steel corrosion. Steel and other metals are used to reinforce concrete structures. We generally refer to the iron reinforcement as rebar, which is short for "reinforcing bar". Steel corrosion leads to the deterioration of concrete structures [18]. Costs of repairs and public safety represent the burden of corrosion of concrete [19]. In 2001, the "Annual direct cost of highway and bridge repairs (largely related to reinforcement corrosion) was \$8.3 billion in the U.S. Alone" [10]. Financial cost of repairing damaged concrete structures may exceed the cost of primary construction [20].

Common causes of rebar corrosion include carbonation, chloride ingress, loss of alkalinity [18]. Chloride ingress and sulfate attack are commonly thought to be serious threats to deterioration of concrete and decreased durability of concrete structures [21]. The main determinant of durability of concrete structures is resistance to chloride ingress [22][23].

One of the most common causes of steel corrosion is chloride ingress. Chloride ingress often occurs as a result of manufacturing materials being contaminated with chloride ions. Manufacturing materials may become contaminated due to exposure to marine water or in cold climates when salt is placed on the concrete to melt ice [18]. This is due to the chemical nature of salt, NaCl, and the disassociation of these atoms in water. Prevention of chloride ions from moving through the cement and corroding steel is a major focus in improving the durability of concrete [19]. Over time the porosity of concrete increases due to the mechanisms described above and can be measured indirectly through weight loss [3].

2.1.4 Importance of Packing Density

An important property of aggregates which affects performance of concrete is the particle size distribution. Particle size distribution of aggregates affects the density at which particles can be packed [24]. Increased particle density improves factors relating to performance of concrete, which include strength, creep, elasticity, and shrinkage. Packing density can be improved by using admixtures. However, the packing density of cement with different admixtures and various proportions of admixtures to cement is difficult to determine using current practices. Current methods for determining particle size distribution do not predict the density at which particle aggregates pack [24].

2.2 Deterioration Mitigation Strategies

Decreasing permeability of concrete may decrease steel corrosion and improve durability of concrete. Permeability of concrete is affected by type of cement, ratio of water to cement and chemical additives, such as silica fume, fly ash, and metakaolin, which are used to decrease pore size of cement [18]. Decreasing the diameter of pore size decreases the diffusion of chloride ions into cement. Additionally, connections between pores and total number of pores influence resistance of concrete to chloride ingress [25].

2.2.1 Concrete Mixtures

The proportion of chemical additives may be changed to enhance the effectiveness of additives in decreasing permeability [18].

In environments high in sulfates, admixtures are commonly recommended to decrease pore size, decrease proportion of C3A to silica, and decrease calcium hydroxide. Additionally, in sulfate-rich environments, the durability of ordinary Portland cement

mortar can be extended by decreasing the effects of sulfate attacks. Researchers suggested that chloride ions may increase the amount of sulfate products that dissolve and increase the formation of Friedel's salt [21]. Unfortunately the techniques described in reducing concrete pore sizes and porosity cannot be applied to already existing concrete structures, only to new structures.

2.2.2 Electrochemical Chloride Extraction (ECE)

Electrochemical chloride extraction (ECE) removes chlorides from reinforced concrete using an electric current [26]. A direct current is induced between the rebar inside the concrete and a titanium mesh placed on the surface of the concrete. The rebar (cathode) is negatively charged and the mesh (anode) is positively charged, causing positively charged particles to move from mesh to rebar, and negatively charged particles to move from rebar to mesh [26].

As chloride ions are negatively charged particles, they are removed from the reinforced concrete. Chloride extraction generally removes up to 40% of the chlorides. Only the free ions in the pore solution are extracted, while bound chloride ions are still left in the concrete. The ECE process is usually performed over a period of 6-12 weeks [26].

2.2.3 Electrokinetic Nanoparticle (EN) Treatment

The process of introducing nanoparticles into concrete with the intent of reducing porosity is referred to as EN treatment. The process results in decreased permeability and increased strength [2][26][27][28]. Work from Dr. Cardenas is the influencing factor for the modeling of the EN treatment. In 2006, 20 nm silica particles and 2 nm alumina particles were utilized in EN treatments reducing the permeability of cement by a factor

of three [28] The movement rate of a charged particle in solution under a direct current is referred to as electrophoretic velocity. Electrophoretic velocity is dependent upon electric current, particle size, zeta potential and possibly other parameters [28]. Although, the simulation requires the electrophoretic velocity to accurately simulate their movement, it does not calculate the electrophoretic velocity but takes the value as an input. The exact calculation of electrophoretic velocity of particles is beyond the scope of this dissertation and is not a feature of the simulation at this time. The electrophoretic velocity of particles utilized in EN treatment were recorded as 2.8×10^{-8} m/s for 20 nm silica particles and 1.3×10^{-7} m/s for 2 nm colloidal alumina under a 39 V/m electric field [27].

Electroosmosis is the term used to describe particle movement through a porous material and will be used interchangeably with electrophoretic velocity or particle velocity in the EN treatment simulation of individual pores.

The EN simulation will be compared with porosity reduction results from actual EN treatments performed by Kunal Kupwade-Patil. Experiments were performed on "cylindrical reinforced concrete specimens" under a variety of conditions. Typically, experiments involved saltwater exposure between control specimens and specimens treated with ECE and EN. ECE and EN treatments typically only were performed for seven days for each experiment, but the saltwater exposure lasted for as long as three years. Specimens were also examined after shorted intervals of saltwater exposures, but unfortunately the process of examination resulted in the destruction of the specimen as required.

There is a large investment of time and effort required to perform these experiments. A simulation of the experiment may be more time efficient and cost effective, while providing more detailed information at the pore level.

2.3 Measurement Techniques

The control and treatment specimens of EN treatment experiments need to be measured in order to determine the effects of EN treatments. Specimens may be tested for many properties described in Section 2.1.2, but for this dissertation, we are only concerned with porosity and pore distribution. Many of the methods used to measure these properties are destructive, therefore multiple samples are taken from individual specimens to be tested. The sample is usually a cross-section of concrete and can be taken from various distances from the rebar and at various sizes. Although the accuracy of the results of these techniques are not without criticism, there needs to be some attempt at comparison between actual results and simulation results. The two techniques utilized are weight loss ratio (WLR) and mercury intrusion porosimetry (MIP).

2.3.1 Weight Loss Reduction (WLR) Method

The WLR porosity measurement method is described by [26] and this section comes completely from that work. Samples are taken from an experimental specimen and powdered to weights of 5 – 7 g and ground to pass a No 30 sieve. In this method, the weight of a concrete sample saturated with water is compared with the weight of the sample when dry. The samples are dried at 105°C. The initial weight of the sample is W_1 and the dried weight is represented by W_2 . Porosity in terms of percentage can be calculated as shown in Equation 3.

$$\text{porosity percentage of sample} = \frac{(W_1 - W_2)}{W_1} \times 100 \quad (3)$$

Thus, the WLR method is a very simple straightforward technique for obtaining porosity percentage of concrete

2.3.2 Mercury Intrusion Porosimetry (MIP)

Mercury intrusion porosimetry (MIP) is the most commonly used technique for determining pore distribution and pore size in cement structures [5]. Several steps are involved in the procedure of MIP. First, a small piece of cement is dried, draining the pores of fluid. The cement sample is placed in a chamber, and mercury is placed around the sample. Pressure is applied to wet the cement with mercury. The most common model is of cylinder-shaped pores, all of which are equally accessible to mercury intrusion. Pressure is increased at intervals, and the movement of mercury into the cement is monitored during each interval. The data for calculating pore size distribution is based on the amount of pressure applied and the volume of mercury introduced into the sample [29].

MIP is useful for providing information about pore size, but does not provide accurate data about pore size distributions. Mercury is unable to access all pores due to shape of some pores and only a small percentage of pores are open directly to the outside of hydrated cement. Therefore, pore size distribution can not be accurately estimated based on MIP [29]. This method does not allow for differentiation between mercury intruding into one long pore or into many short pores. It has been found that the model does not accurately demonstrate pore size distribution. MIP indicates that pores are smaller than they actually are, due to mercury being unable to access pores that are very small or isolated. Models have indicated that some pores are 10 to 100 times smaller

than the actual size of the pores [29] Pore size distribution is typically determined by mercury porosimetry (MIP) Pore size distribution is difficult to determine based on MIP [30] MIP does not provide an accurate characterization of pore structure or total porosity [29][30][31]

All mercury intrusion porosimetry (MIP) data utilized in this paper were performed by Kunal Kupwade-Patil on powdered samples using a Micromeritics Autopore IV 9500 A maximum pressure of 226 MPa was applied in the MIP measurement Currently the Micromeritics Autopore IV 9500 is no longer functional

CHAPTER 3

MODELING AND SIMULATION METHODS

In this chapter we will cover the broad topics of modeling and simulation. For modeling, we will discuss the history of sphere packing and the chemistry that is involved in our models. We will also discuss previous methods and proofs related to this packing problem.

3.1 Modeling

Modeling is used to describe a process or event in a formally written way. When examining models of processes, it is important to understand that the model is an illustration of the process and not a determinant of it. For example, if we correctly implement all the rules that we are aware of in regards to a given process, but our model results do not conform to the analytical results, we can infer that there is a component missing from our understanding. The process being modeled may be simple or complex, but even simple models can provide insight into the examined processes. Examples of processes in which modeling was used include the equation for gravity, and how the HIV virus causes AIDS in patients [32].

We model the electrokinetic nanoparticle (EN) treatment to study the reduction of porosity in concrete at a pore level. Information gained from modeling may reduce time

requirements, increase porosity reduction and improve cost efficiency for ultimately electrokinetic nanoparticle treatments [27]

3.2 Sphere Packing

Sphere packing, as the name suggests, is the packing of spheres into either bounded or unbounded spaces. We will give a short history of the history of sphere packing as well as the categorization of sphere packing methods.

3.2.1 History

Kepler's conjecture proposes that the maximum packing density of mono-sized hard spheres in three-dimensional space is given in Equation 4

$$\frac{\pi}{\sqrt{18}} \approx 0.74048 \quad (4)$$

The Kepler conjecture has been proven to be true if the spheres are arranged in a regular lattice [33]. That is, a pattern is repeated exactly to pack a given space. Thus the only possible counterexample would be a packing without a repeating pattern. In the twentieth century, Claude Ambrose Rogers was able to prove an upper bound of 78%. Although a higher bound than Kepler's conjecture, we can be certain of this absolute bound. In 2003, Hales published a computational proof of Kepler's conjecture in the Annals of Mathematics. A computational proof of the analysis indicates that the proof is correct. The Flyspeck project was started to formalize the proof completely [34].

As a result, any packing density for mono-sized spheres greater than 78% should be rejected outright and packing densities higher than 74.048% should be viewed with great suspicion. Furthermore, we are primarily considering sphere packing with two sets of spheres. Each sphere in a given set is the same size, but the sets do not contain spheres

of the same size To clarify, we are packing with two different sizes of spheres In this case, we can be assured of an absolute bound of $78\% + 22\% * 78\% = 95.16\%$ That is the packing density of a large sphere size of 78% and the packing density of the unpacked space, 22%, with a smaller sphere size Considering Kepler's Conjecture instead, we obtain an upper bound of $74.048\% * 25.952\% * 74.048\% = 93.265\%$ This bound holds no matter how small the size of the smaller sphere set In our simulations, we expect to obtain much lower bounds for two reasons First, we are packing a bounded space, thus the spheres may not be able to fit in the available space due to topological reasons, even if the mathematical calculations indicate there is enough total space available Second, we will not be using a structured packing in a non-bounded space We have bounds that are not allowed to intersect the spheres, thus we do not count partial spheres as many previous methods Furthermore, we are randomly packing, so there is no effort made to consciously pack spheres as close as possible There are two types of packing found in molecular structures that approach the maximum mono-sphere packing bound hexagonal close packing (HCP) and face centered cubic (FCC) packing

3.2.2 Categorization

Random packing can be categorized into random loose packing (RLP) or random close packing (RCP) [35] Random loose packing traditionally implies that particles are packed with some constant force such as gravity The difference between the two methods is that random close packing involves shaking or some other temporary force applied to increase the density of a random loose packing Previously experiments in literature result in an average density of 55% for random loose packing and 64% for random close packing [35]

3.3 EN Model

Concrete pores are modeled as cylinders [5] To decrease time of simulation, nanoparticles are modeled as hard spheres [36] This simulation work would still be valuable for modeling non-spherical nanoparticles as the non-spherical nanoparticles could be bounded by a bounding sphere for broad phase collision detection purposes [37] The simulation algorithms and model still hold in the case of non-spherical nanoparticles, but the collision detection would need to be extended to compensate for the change

3.3.1 Coordinate System

We will describe the methods used to pack differently sized spheres into a cylindrical space We create our objects in three dimensional space with x , y and z representing each dimension The coordinates represent three dimensional space as follows Using this page as a reference, x would represent left and right, y would represent up and down, and z would represent moving towards or away from the page For the x -axis, the left direction is negative and the right direction is positive For the y -axis, up is considered negative and down is considered positive For the z -axis, moving closer to the page is considered a negative movement and moving away from the page is negative (Figure 3 1)

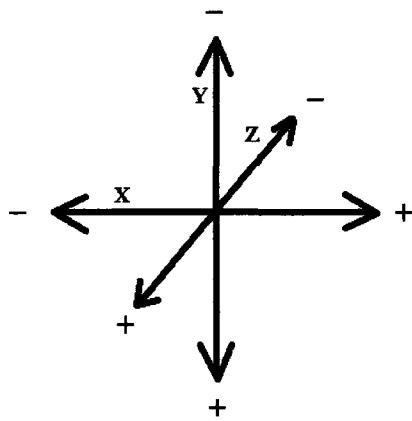


Figure 3 1 Model co-ordinate system

3.3.2 Sphere Model

In particular, we are interested in packing a bounded three-dimensional space with two sets of spheres of different sizes, say sphere set A with diameter A_D and sphere set B with diameter B_D . A sphere from either set will be represented by S . The diameter D of sphere S will be represented by S_D . If $S_D = A_D$, then S belongs to set A . If $S_D = B_D$, then S belongs to set B . We will use R to represent radius when mathematically convenient, where the radius of sphere S is S_R .

$$S_R = \frac{S_D}{2} \text{ for any sphere } S \quad (5)$$

We will refer to a sphere's location by the point at the center of the sphere S_c . As S_c is a point in three-dimensional space, it has an x , y , and z coordinate which we will refer to as S_x , S_y and S_z respectively.

3.3.3 Partial Sphere Volume

It is useful to be able to calculate partial sphere volume. We only present partial sphere volume for a sphere that is intersected by at most two planes. We utilize the disc method to sum cylindrical slices of the sphere between two xz-planes. As all spheres are circular, they revolve around axes parallel to the y-axis. We determine the boundary of the intersecting planes as the boundary between sectors when moving on the y axis. This can also be applied to the COI method, as xz-planes give boundaries for the COI. The top of the cylinder is also congruent to a xz-plane, and we can accurately calculate partial sphere volume of spheres that are not fully contained. The equation for a sphere of radius R is given in Equation 6,

$$R^2 = x^2 + y^2 + z^2 \quad (6)$$

We take xz-slices of the sphere which have an area given in Equation 7 where r is the radius of each slice,

$$V = \pi r^2 \quad (7)$$

For each slice r changes depending on the location along the axis for the sphere as described in Equation 8,

$$r^2 = R^2 - y^2 \quad (8)$$

We then take the integral of the slices over the desired area of the sphere shown in Equation 9,

$$\int_a^b \pi (R^2 - y^2) dy \text{ where } R \geq b > a \geq -R \quad (9)$$

Solving for the integral results in Equation 10,

$$V = \left(\pi R^2 b - \frac{\pi}{3} b^3 \right) - \left(\pi R^2 a - \frac{\pi}{3} a^3 \right) \quad (10)$$

Substituting $b = R$ and $a = -R$, we obtain the equation for the volume of a sphere as expected in Equation 11,

$$V = \left(\pi R^3 - \frac{\pi}{3} R^3 \right) + \left(\pi (R^3) - \frac{\pi}{3} R^3 \right) = \frac{4 \pi R^3}{3} \quad (11)$$

3.3.4 Cylinder Model

A cylinder C closed at one end is created with a diameter C_D and height C_H . For simplicity, we may use cylinder radius C_R as desired where

$$C_R = \frac{C_D}{2} \quad (12)$$

We will refer to the closed end of the cylinder as the base of the cylinder. The base of the cylinder represents the end of the pore where it may terminate with rebar. The y-axis passes through the center of the base and is also perpendicular to the base. The open end of the cylinder is centered at $(0, 0, 0)$. We will refer to the open end of the cylinder as the top of the cylinder (Figure 3.2). Spheres are assumed to flow from above the xz-plane congruent with the top of the cylinder. This area may either represent the area outside of the concrete or it may represent another pore that feeds into our own pore represented by C . The remaining curved boundary of the cylinder will be referred to as the side of the cylinder.

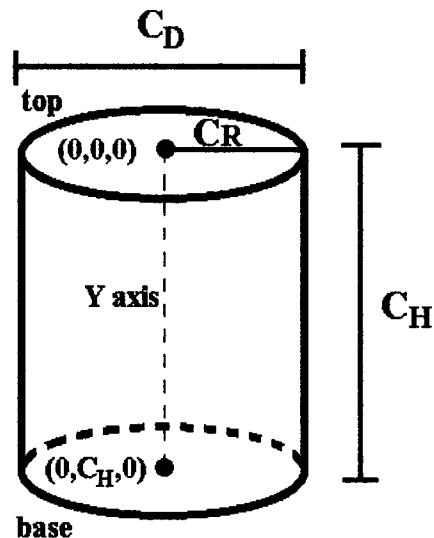


Figure 3 2 Representation of a pore as a cylinder

We add spheres to the cylinder from the top of the cylinder. The large spheres of set A are introduced and packed first before the smaller spheres of set B are introduced. In order to simulate the movement of spheres due to electrokinetic forces, we must check for collisions. A sphere must not violate the the cylinder wall or boundaries of other spheres.

3.3.5 Solution Percent Weight to Volume Conversion

In the literature and practice, references to the amount of particles added to solutions are given as a weight percentage. All calculations utilized in the simulation require instead a volume percentage. In order to accurately model a given solution, we must be able convert from a weight percentage to a volume percent. The weight percentage is the percent of a solution's total weight taken by the solute. For example, experiments conducted by Kupwade-Patil used a 12% 20 nm particle solution by weight [26]. The simulation does not consider weight, but only volumes of particles. In order to

simulate pore packing similar to empirical data, we must convert weight percentage values to volume percentage values. We will consider particle mass instead of weight, as weight is simply mass times gravity

$$\text{weight} = (\text{mass})(\text{gravity}) \quad (13)$$

$$\text{mass} = (\text{volume})(\text{density}) \quad (14)$$

$$\text{volume} = \frac{\text{mass}}{\text{density}} \quad (15)$$

We will follow the convention of the particles being referred to as solute, the liquid they are suspended in as solvent, and the combination of solute and solvent as solution

In order to calculate the percent weight of particles in solution divide the weight of the particles by the weight of the particles and solution combined. Let W_p be the weight of a given set of particles. Let W_s be the weight of the solvent in which the particles are suspended. Let P_w represent the percent weight which is defined in Equation 16

$$P_w = \frac{W_p}{W_p + W_s} \quad (16)$$

Substituting Equation 13 into Equation 16 results in Equation 17. Let M_p represent the mass of the particles, M_s represent the mass of solution and G represent gravity. G cancels and we obtain Equation 18

$$P_w = \frac{M_p G}{M_p G + M_s G} \quad (17)$$

$$P_w = \frac{M_p}{M_p + M_s} \quad (18)$$

Again, we substitute, this time with Equation 14 Let V_p represent the volume of the particles, D_p represent the density of the particles, V_s the volume of solution, and D_s the density of solution We obtain the following Equation 19,

$$P_w = \frac{V_p D_p}{V_p D_p + V_s D_s} \quad (19)$$

We note that the total volume of the solution is the combined weight of particles and solution Let V_t represent total volume of the solution with particles suspended as shown in Equation 20,

$$V_t = V_p + V_s \quad (20)$$

We wish to obtain the percent volume for the particles which we will represent with P_v as defined in Equation 21,

$$P_v = \frac{V_p}{V_t} \quad (21)$$

For convenience, we also need the percent volume of solute as defined in Equation 22,

$$P_{vs} = \frac{V_s}{V_t} \quad (22)$$

Note also that the percent volume of solvent must be $P_{vs} = 1 - P_v$ Multiplying Equation 19 by V_t/V_t results in Equation 23,

$$P_w = \frac{P_v D_p}{P_v D_p + (1 - P_v) D_s} \quad (23)$$

Solving for P_v results in Equation 24,

$$P_v = \frac{D_s}{\frac{D_p}{P_w} + D_s - D_p} \quad (24)$$

We can plug in values that correspond to experiments as appropriate A 12% by weight aluminum particle solution can be converted into percent volume given that the density of water is 0 9982071 g/cm³ at 20° C and the density of aluminum is 2 698 g/cm³ at 20° C Densities at other temperatures can be obtained from external sources, but 20° C is a standard value Substituting and solving, we obtain Equation 25,

$$P_v = \frac{99827}{\frac{2698}{0.12} + 099827 - 2698} = 0.0480 \text{ or } 4.8\% \quad (25)$$

So a 12% by weight aluminum solution is 4.8% by volume Generally since metals are more dense than water, they will have a lower volume percentage than weight percentage

3.4 Simulation

A simulation is the implementation of a model as a computer program [38] The complexity of the program generally correlates to the complexity of the model [32] A vague model will require assumptions to be made when implementing it as software It is also important to note that not all models can properly be implemented on current computer systems It is certainly impossible to hold an infinite amount of space, so all problems must be either practically finite in nature, or there must be a method of dealing with the infinities [39] This is the basic issue that prevents a computer from being categorized as a universal Turing machine [40] It is also important to note, that even when it is theoretically possible to implement a model as a simulation, the problems that are simulated can be intractable

3.4.1 How Computer Simulation Can Help

Computational simulations have been used to model functions of real objects [41] Since the 1980's, computers have been used in modeling 3-dimensional objects in construction design [42] This may decrease the time and cost of modeling and experimenting [41] Computer simulations help identify potential design flaws, allowing engineers to correct potential problems prior to initiating construction projects Computer simulations in construction decrease production cost and increase productivity Visualization of construction projects through computer modeling may provide information to engineers that would be difficult to determine through sole reliance on Equation [42]

3.4.2 Asymptotic Complexity

In this paper, we redesign the electrokinetic nanoparticle (EN) treatment simulation to reduce the time requirements at the expense of additional memory That is, our sectoring implementation runs significantly faster using a nominal increase in memory This will be described later in detail, but it will be necessary to understand asymptotic complexity as a basis for comparison For this paper, all references to asymptotic complexity will be in terms of time, unless specifically noted We will also adhere to the computer science standard of $\log_2 N$ being written as $\log N$

Asymptotic complexity is a formal method of describing the amount of resources a program requires in time or computer memory Both time and memory are considered independently and the complexity of each on a given program need not be identical We base our assessment on the number of objects that are entered into an algorithm which we represent as N Also, an arbitrary constant c serves to partition algorithms of similar

growth rates into the same classes Typical growth rates include c , $\log_2 N$, $(\log_2 N)^2$, N , $N \log N$, N^2 , N^3 and 2^N from least costly to most costly [43] Note that $\log N$ in this case is base two according to computer science standard notation, Thus $\log_2 N$ is written as $\log N$ as a standard convention in computer science Other functions such as N' and N'' can be used and the list is not exhaustive For demonstration purposes, let us consider two algorithms one that takes $1000 N$ steps to complete and the other $10 N^2$ steps If N is small then, $10 N^2$ is smaller, but eventually $10 N^2$ will become larger than $1000 N$ as N becomes large [44] For a practical example, assume that we must sort 100 comparable objects, thus $N = 100$ Commonly used sorting algorithms, such as selection sort, are well known to take less than $c N^2$ steps which would take at most $c 100 100 = 10,000 c$ steps to sort the 100 objects for some arbitrary constant c [45] A faster general sorting algorithm, mergesort, takes approximately $c N \log N$ steps, so to sort 100 object would take at most $c 100 7 = 700 c$ steps for an arbitrary constant c As a result, you can see that the higher order equation takes many more steps than the lower order equation where the arbitrary constant c is not dissimilar The constant c becomes less important as N becomes large, and is generally ignored for comparison purposes

Let $T(N)$ represent the number of steps an algorithm must take to solve a problem given N objects Let $f(N)$, $g(N)$, $h(N)$ and $p(N)$ arbitrarily represent a single term growth rate based on N , most likely from the typical growth rates discussed earlier

The formal definitions, according to [43] are

Definition $T(N) = O(f(n))$ if there are positive constants c and n_0 such that

$$T(N) \leq cf(N) \text{ when } N > n_0$$

Definition $T(N) = \Omega(g(n))$ if there are positive constants c and n_0 such that $T(N) \leq cg(N)$ when $N > n_0$

Definition $T(N) = \Theta(h(n))$ if and only if $T(N) = O(h(N))$ and $T(N) = \Omega(h(n))$

Definition $T(N) = o(p(n))$ if $T(N) = O(p(N))$ and $T(N) \neq \Theta(p(n))$

The equal sign for asymptotic notation is prevalent in computer science, but mathematicians prefer to use the \in symbol to acknowledge that $O(f(n))$, $\Omega(g(n))$, $\Theta(h(n))$ and $o(p(n))$ are sets $O(f(n))$, read "Big Oh", is the set of all functions that do not exceed the function $f(n)$ times an arbitrary constant This is considered to represent the worse case growth of an algorithm and is the most commonly used measure $\Omega(g(n))$, read "big omega", is the set of all functions that grow at least as fast as $g(n)$ times an arbitrary constant Big omega is often considered a best case scenario, describing the minimum growth of an algorithm $\Theta(h(n))$, read "big theta" is the set of all functions that are bound above and below by the same function $h(n)$ times an arbitrary constant that can be different for the upper and lower bound $o(p(n))$, read "little oh", is the set of all functions that are bound above by a function $p(n)$ times an arbitrary constant, but cannot be bound below by the same function times an arbitrary constant

Only the highest term should be included, $O(N^2+N)$ would not be written as such and instead be considered as $O(N^2)$ Constants are also not included in the notation, as they are accounted for in the definition Thus, we would not write $O(5N^2)$, but instead we write $O(N^2)$ Higher order functions can be quite costly in terms of time and memory If an algorithm to solve a problem takes more memory than is reasonably available or cannot solve a given problem in a reasonable amount of time, we refer to the problem as

intractable. Most algorithms work with a small number of objects, but problems can quickly become intractable if N becomes large.

3.4.3 Time

When simulating the electrokinetic process, there are several timescales. There is the amount of time that a simulation will take to complete. We will refer to this as real time to be consistent with the time command on Linux. In the simulation, particles are being packed into a pore and time is progressing. We will refer to this time as simulation time. There is no simple equation to convert between real time and simulation time. This is due to the fact that the relationship between simulation time and real time varies based on the number of particles being considered.

In the simulation, we use the term time-step to describe each time we move every particle a set distance. Each time-step can be converted directly to simulation time, but the amount of real time for the time-step varies depending on the number of particles to be moved. To convert a time-step to simulation time, we must know the particle speed and the particle distance moved each time-step. Each time-step will take simulation time as determined by Equation 26

$$TS_{st} = \frac{P_M}{P_S} \quad (26)$$

The terms TS_{st} is used to represent the simulation time for a time-step, P_S is the particle speed and P_M is the particle movement distance in a time-step. P_S should be in nanometers per second and P_M should be in nanometers. Typically P_M will be a fraction of P_S . Solving Equation 23 for P_M , we obtain Equation 24

$$P_M = TS_{st} P_s \quad (27)$$

When graphics are enabled, additional constraints are added In order to have smooth animation, 30 frames per second are desirable In this case, each time-step must complete in approximately 33 ms including the time required to draw the particles and pore In practice, if the time required for a time-step is less than 33 ms, the simulation remains idle for the unused time If the time required for each time-step is more than 33 ms, the simulation will visibly slowdown According to previous work, 20 nm particles were moved at 100 nm/s This is equivalent to 0.1 nm/ms

Substituting into Equation 27 results in Equation 28

$$P_M = 33 \text{ ms} \frac{0.1 \text{ nm}}{\text{ms}} = 3.3 \text{ nm} \quad (28)$$

Therefore at 30 frames per second, moving particles at 3.3 nm per time-step, we achieve equality between real time and simulation time Increasing the particle movement speed increases the time of each time-step according to Equation 26 which translates to a faster simulation relative to real time The issue with increasing particle movement rates too high is a lack of authenticity if the values become too large For example, a particle could potentially bypass blocking spheres to enter a gap that was impossible to reach

3.4.4 Cylinder Boundary Collision Detection

We first describe the conditions under which a sphere S is contained within a cylinder C For convenience, we define S_{yd} as the distance from sphere S to the y-axis as shown in Equation 29

$$S_{yd} = \sqrt{S_x^2 + S_z^2} \quad (29)$$

We note that a sphere contained within C may be partially contained or fully contained within C . In our simulation, spheres that are not at least partially contained within C as per Equation 30 will be deleted when detected.

$$S_{yd} \leq C_R - S_R \text{ and } C_H + S_R \leq S_y \quad (30)$$

A partially contained sphere may extend beyond the opening of the pore at the xz-axis, as the plane represents the boundary between the pore and the area external to the pore. On the other hand, a fully contained sphere adheres to Equation 31

$$S_{yd} \leq C_R - S_R \text{ and } C_H + S_R \leq S_y \leq S_R \quad (31)$$

Clearly, any sphere that is fully contained is at least partially contained, but the converse is not necessarily true. Any sphere that is not partially contained within the cylinder will be deleted. Figure 3.3 visualizes these boundaries in a simplified two-dimensional side view. In Figure 3.3, the left illustration shows fully contained sphere A, partially contained sphere D, and non-contained spheres B, C and E. On the right is an illustration of the variables C_R , S_{yd} and S_R for any vertical cross-section of a cylinder containing both the y-axis and a sphere to be checked for containment.

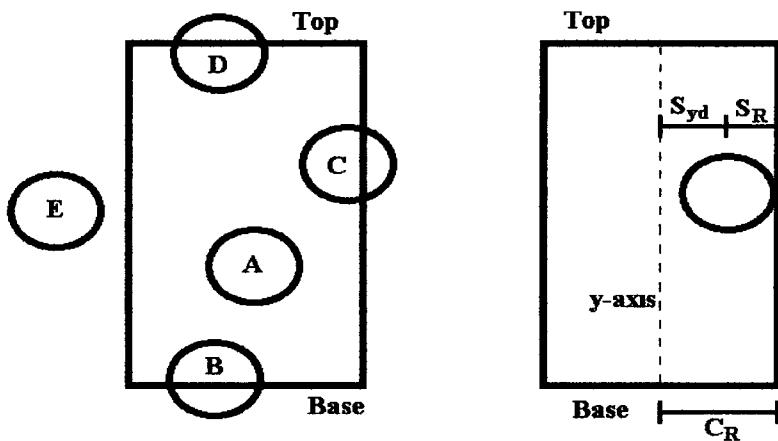


Figure 3.3 Side view of a cylinder for containment

3.4.5 Sphere Collision Detection

Collision detection between objects can be divided into two phases narrowphase and broadphase [46][47] Broadphase collision detection refers to the decision of determining which objects to test for collisions Narrowphase collision detection refers to testing for collisions between individual objects In this section, we will present only the narrowphase collision detection For a discussion of broadphase collision detection, please refer to Section 3 6

To check a collision between spheres we compare the sum of the sphere radii to the distance between their center points Assume a sphere S_1 with radius S_{1R} and another sphere S_2 with radius S_{2R} and sphere centers $S_{1c} = (S_{1x}, S_{1y}, S_{1z})$ and $S_{2c} = (S_{2x}, S_{2y}, S_{2z})$ Let $d(S_1, S_2)$ be the non-negative distance function between sphere centers S_{1c} and S_{2c} In other words

$$d(S_1, S_2) = \sqrt{(S_{1x} - S_{2x})^2 + (S_{1y} - S_{2y})^2 + (S_{1z} - S_{2z})^2} \quad (32)$$

If $d(S_1, S_2) \geq S_{1R} + S_{2R}$ then there is no violation of sphere boundaries with equality indicating that the spheres are touching Otherwise, if $d(S_1, S_2) < S_{1R} + S_{2R}$ then the spheres intersect and the boundaries are violated

In Figure 3 4, we illustrate the non-collision of spheres in A, the touching of spheres in B and the collision of spheres in C

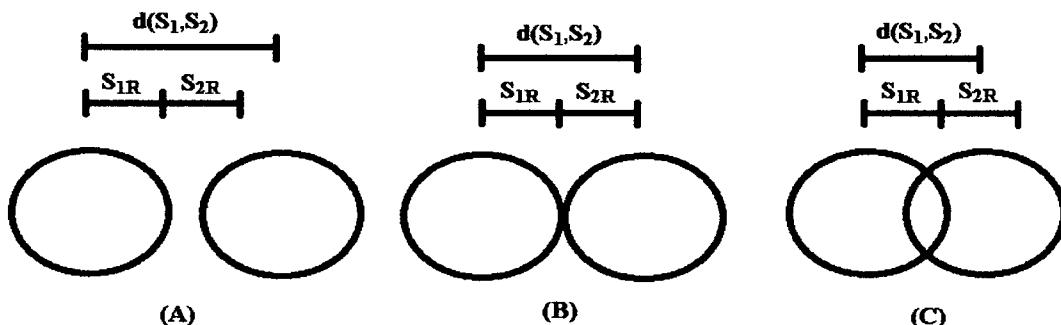


Figure 3 4 Sphere interaction determination

We illustrate the relationship between these collision states and the distance of spheres compared to the sum of their radii. Spheres with different radii are compared in the exact same manner with no changes necessary. In practice, the simulation avoids a square root operation by squaring both sides of Equation 32. Note also, that even though a sphere technically can collide with itself according to Equation 32, we will not consider such an incident a collision and will avoid testing a sphere for collision against itself.

3.4.6 Sphere Introduction

Spheres are generated in the xz-plane around the origin so that they are within the bounds of the cylinder mouth. The center of a sphere S that is introduced will be on the xz-plane, or in other words, $S_y = 0$. S_x and S_z are chosen such that S is partially contained in cylinder C . For example, choose S_x such that an S_z exists where the sphere is partially contained in C . The limits for this are described to Equation 33

$$-C_R + S_R \leq S_x \leq C_R - S_R \quad (33)$$

Given a random valid S_x , we choose a random S_z such that S is partially contained within C as per Equation 34

$$-\sqrt{((C_R - S_R)^2 - S_x^2)} \leq S_z \leq \sqrt{((C_R - S_R)^2 - S_x^2)} \quad (34)$$

Figure 3.5 illustrates the top of the cylinder with valid S_x domain marked with a solid horizontal line. Once S_x is chosen randomly, the valid S_z range is a vertical line bounded by the dashed circle. Note that if the S_x domain is broken into n equal partitions, the areas of the dashed circle related to these partitions are not equal. As a result, some partitions of the dashed circle have a higher probability to contain a sphere per unit area.

than other partitions In order to mitigate this effect, we alternate S_x and S_z as the independent and dependent variables each time a new sphere is introduced

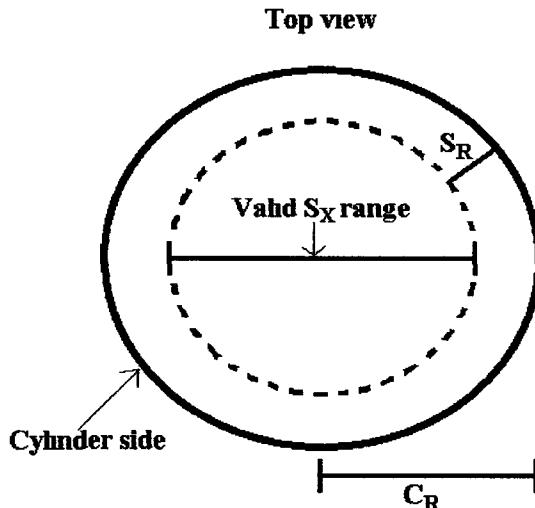


Figure 3.5 Particle introduction range

3.4.7 Sphere Movement

Two types of motion are simulated vertical movement and horizontal movement
Downward movement is any motion with a vertical component Sideways movement is motion with no vertical component

In Figure 3.6, the top view of the sphere illustrates the eight directions that a particle can move horizontally The side view illustrates the difference between the vertical and horizontal directions For each horizontal direction, there is a related vertical direction that also contains a vertical component In addition, vertical motion also contains motion straight down, represented by the arrow pointing straight down There are nine vertical movement directions and eight horizontal movement direction available for a total of 17 possible movements The vectors to represent the 17 possible movements is referred to as M_T M_T contains disjoint subsets M_V and M_H where M_V is the

set of vectors with a vertical component and M_H is the set of vectors with no vertical component. Each vector M is composed of three real number values M_x, M_y and M_z . The vectors to represent these movements are listed in Table 3 1.

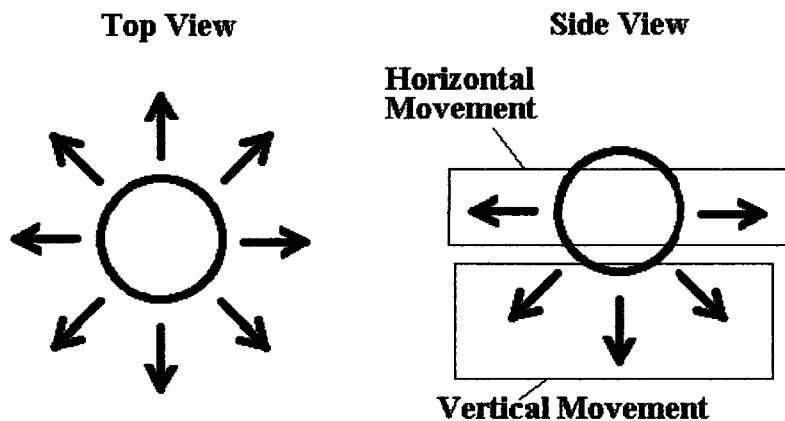


Figure 3 6 Sphere movement directions

Table 3 1 List of movement vectors

Vertical Motion (M_x, M_y, M_z)	Horizontal Motion (M_x, M_y, M_z)
(0 707106, 0 707106, 0 0)	(1 0, 0 0, 0 0)
(-0 707106, 0 707106, 0 0)	(-1 0, 0 0, 0 0)
(0 0, 0 707106, -0 707106)	(0 0, 0 0, -1 0)
(0 0, 0 707106, 0 707106)	(0 0, 0 0, 1 0)
(0 577350, 0 577350, 0 577350)	(0 707106, 0 0, 0 707106)
(0 577350, 0 577350, -0 577350)	(0 707106, 0 0, -0 707106)
(-0 577350, 0 577350, 0 577350)	(-0 707106, 0 0, 0 707106)
(-0 577350, 0 577350, -0 577350)	(-0 707106, 0 0, -0 707106)
(0 0, 1 0, 0 0)	No Movement

The magnitude of each of the vectors of Table 3 1 is one. This ensures that particle movement will be consistent regardless of direction chosen. In order to move a particle S , we create a new sphere S_N by performing a translation on the center of S with a

movement vector M scaled by the particle movement rate S_R [48][49] We must scale the vector by the particle movement rate S_R to reflect the electrophoretic velocity S_V input into the simulation The translation equation is shown in Equation 35 In order to process the vector multiplication and addition of Equation 35, we must evaluate S_x , S_y and S_z separately as shown in Equations 36 to 38

$$S_N = S_c + S_R M \quad (35)$$

$$S_{Nx} = S_x + S_R M_x \quad (36)$$

$$S_{Ny} = S_y + S_R M_y \quad (37)$$

$$S_{Nz} = S_z + S_R M_z \quad (38)$$

We create the new particle S_N instead of modifying the coordinates of S , in case the particle movement results in a collision If a collision occurs between S_N and any sphere other than S , or the sphere S_N is not partially contained, we immediately delete S_N and no movement has occurred Otherwise, we delete S and then relabel S_N as S This gives the appearance that S has moved only when such movement would not result in a collision Psuedocode can be found in Table 3 2

Table 3 2 Psuedocode for particle movement

A1	Pick an unused vector V at random from V_M
A2	Generate a new sphere S_N at the given position based on S and V
A3	If S_N has a collision, then the movement failed
3 1	Delete S_N
3 2	Remove vector V from consideration in V_M
A4	Otherwise the movement succeeded
4 1	Delete S
4 2	Go to step A6
A5	If V_M is empty, go to step A6
5 1	Otherwise go to step A1
A6	Return movement success or failure

3.5 Methods

There are multiple algorithms that have been tested for the simulation of the electrokinetic nanoparticle treatment. We will discuss several methods, but focus on the brute force method, the cylinder of influence (COI) method and sectoring method. Generally, each simulation uses a cylinder to represent a pore of a certain size and spheres to represent nanoparticles being inserted to reduce the pore volume. During the simulation, these particles are constrained to follow simple physical collision rules. The particles must respect the boundary of the cylinder. This means that if any part of the particle violates the cylinder wall it can not be used in calculating the porosity reduction. Also each particle is not permitted to intersect with any other particle. These collisions

are tested continuously by using the position and radius of the particles and the radius and height of the cylinder

During the simulation, spheres are added in order of decreasing diameter. Porosity reduction is calculated as the volume of added particles completely within the cylinder divided by the cylinder volume. The simulation is capable of adding chloride ions as normal particles. Our chloride ions would be modeled as solvated chloride ions that are represented as 0.6 nm spheres.

3.5.1 General Simulation Method

We will describe the general algorithm for EN treatment simulation of a pore. The simulation begins by initializing variables and data structures as per step A1. We will refer to the single completion of step A2 and step A3 as a time-step. This is the smallest divisible unit of time that is distinguishable. The movement rate of a sphere is the distance it will travel in a single time-step if the sphere moves. The magnitude of each movement vector evaluates to one. General pseudocode is written under Table 3.3.

Table 3 3 General simulation method

A1 Initialize variables
1 1 Diameter and height of the cylinder
1 2 List of different sphere sizes
1 3 Arrays of vectors of movement directions
1 4 Method specific structures
A2 Introduce a constant number of spheres to the cylinder
2 1 Check each inserted sphere A for collisions with other spheres
2 1 1 If a collision occurs, delete A
A3 For each sphere A, attempt to move A
3 1 Set $V_M=V_V$ and attempt vertical movements
3 2 If all vertical movements of 3 1 failed
3 2 1 Set $V_M=V_H$ and attempt horizontal movements
A4 Return to step 2 unless the simulation is complete

In each time-step, there is a particle introduction phase of step A2 and a movement phase of step A3. Particles are introduced in step A2 as per Section 3 4 6. Specific implementation details for the specific methods will be described in Sections 3 6 1, 3 6 2 and 3 6 3. The movement phase of step A3 involves the movement of particles described in Section 3 4 7. This phase requires multiple steps. First, the electrokinetic force on the particles is simulated as a downward motion from the mouth of the cylinder to the base of the cylinder. A finite displacement is defined for the distance that a particle was to move per unit of time, and per simulation cycle. The simulation checks up to nine downward positions, one at a time, in the particle movement direction.

to see if the particle can move without violating the space of another particle or the cylindrical wall. The order in which these directions are checked is random, and the first valid position is selected. If no downward motion is possible, the eight sideways motions are checked in the same manner. If all attempts to move the particle fail, then it remains in place. This process may be visually displayed in 3-D using OpenGL. For a platform independent GUI window, GLUT was originally used, but FreeGLUT is used in the latest versions. At the time of this writing, the graphical version is only available for the Windows operating system.

3.5.2 Fixed Spheres

During the course of the simulation, individual spheres will no longer be able to move for the rest of the simulation. This is likely due to other spheres packing closely around and preventing movement. The boundaries of the cylinder may also contribute to preventing sphere movement in conjunction with other spheres. Attempting to move any sphere that is incapable of movement due to obstruction is futile, yet takes computational time. In point of fact, attempting to move a sphere that is incapable of movement is more expensive than attempting to move a sphere capable of movement.

A sphere incapable of movement must test all 17 movement directions in order to determine that a sphere cannot move. On the other hand, a sphere capable of movement may succeed on the first movement attempt. If we assume that we may have n successful movement vectors with equal probability, then we can calculate the probability of selecting a vector in the k^{th} attempt that will not result in a collision. Table 3.4 gives the conditional probabilities for each possibility as well as $E(k|n)$, the expected value of k given n . The values were calculated in OpenOffice Calc. The values are only shown to

two decimal places and the zero values are simply < 0.01 , but are non-zero values that OpenOffice Calc utilizes at an unknown higher precision. Assuming that each non-zero value of n has an equal chance of occurring we average $E(k|n)$ for all n to obtain $E(K) = 2.64$. Thus, immovable spheres are much more expensive where $E(0) = 17$.

Table 3.4 Conditional probabilities of choosing a successful vector on the k th attempt

n	k																$E(k n)$
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	
1	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	0.06	9
2	0.12	0.11	0.1	0.1	0.09	0.08	0.07	0.07	0.06	0.05	0.04	0.04	0.03	0.02	0.01	0.01	6
3	0.18	0.15	0.13	0.11	0.1	0.08	0.07	0.05	0.04	0.03	0.02	0.01	0.01	0	0	0	4.5
4	0.24	0.19	0.15	0.12	0.09	0.07	0.05	0.04	0.02	0.01	0.01	0	0	0	0	0	3.6
5	0.29	0.22	0.16	0.12	0.08	0.05	0.03	0.02	0.01	0.01	0	0	0	0	0	0	3
6	0.35	0.24	0.16	0.1	0.06	0.04	0.02	0.01	0	0	0	0	0	0	0	0	2.57
7	0.41	0.26	0.15	0.09	0.05	0.02	0.01	0	0	0	0	0	0	0	0	0	2.25
8	0.47	0.26	0.14	0.07	0.03	0.01	0	0	0	0	0	0	0	0	0	0	2
9	0.53	0.26	0.12	0.05	0.02	0.01	0	0	0	0	0	0	0	0	0	0	1.8
10	0.59	0.26	0.1	0.04	0.01	0	0	0	0	0	0	0	0	0	0	0	1.64
11	0.65	0.24	0.08	0.02	0.01	0	0	0	0	0	0	0	0	0	0	0	1.5
12	0.71	0.22	0.06	0.01	0	0	0	0	0	0	0	0	0	0	0	0	1.38
13	0.76	0.19	0.04	0.01	0	0	0	0	0	0	0	0	0	0	0	0	1.29
14	0.82	0.15	0.02	0	0	0	0	0	0	0	0	0	0	0	0	0	1.2
15	0.88	0.11	0.01	0	0	0	0	0	0	0	0	0	0	0	0	0	1.13
16	0.94	0.06	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1.06
17	1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	1
																	Average 2.64

Also, we must consider downward movement differently than horizontal movement. A sphere will only be able to have at most a constant number of downward movements. A sphere will certainly eventually be prevented from downward movement by the base of the cylinder if not earlier by other spheres. It is important to realize that a sphere may not be completely immobilized and still oscillate horizontally, but nevertheless never be able to make another downward movement due to neighboring spheres or the cylinder base. If we allow such spheres to oscillate indefinitely, they will take processor time, but may be irrelevant for the packing of other particles. Figure 3.7

illustrates a potential situation where sphere A oscillates between two positions denoted by the solid and dashed sphere. Surrounding sphere A are spheres that can no longer move represented by the shaded circles. In this scenario, sphere A will always have a movement choice, thus sphere A will always move despite the fact that the movement can have no effect on the surrounding spheres or the overall porosity.

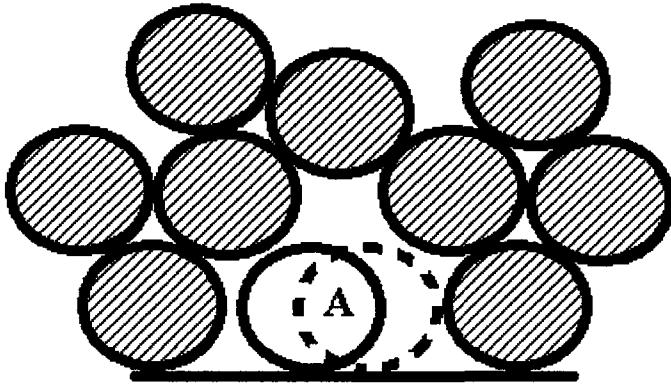


Figure 3.7 Sphere A oscillating between two locations

To reduce the number of calculations that are performed, we eliminate spheres from consideration for movement if it is determined that they will be unlikely to have any future vertical movements. We refer to this as fixing the sphere, and after being fixed, the sphere is a fixed sphere. The decision to fix a sphere is based on a positive integer stored for each sphere referred to as the fix counter. The fix counter is initialized at zero for each sphere and is reset to zero for any sphere that successfully completes a vertical movement. If the fix counter is greater than or equal to a critical fix value, then the sphere will become fixed. The critical fix value can be adjusted in the program code, but the author has chosen it to be 1000. The fix counter may be incremented in three distinct scenarios: 1) attempting to move an immobile sphere will increment the sphere's

fix counter by a constant amount we will refer to as the fix score for immobile spheres or *FSI*, 2) Attempting to move a sphere that cannot move vertically, but can move horizontally will increase the fix counter by a different constant amount we will refer to as the fix score for horizontal only spheres or *FSHO* or 3) The sphere contacts the base of the cylinder, which we refer to as "bottoming out", and the fix counter will be increased by the fix score for bottoming out or *FSBO*. *FSI*, *FSHO* and *FSBO* do not have a predetermined values and can be adjusted in the program code. There is no option in the current simulation to fix a sphere due to contact with the side of the cylinder. The author has chosen $FSI = 10$, $FSHO = 1$ and $FSBO = 10$ for current simulation values. An immobile sphere or sphere that contacts the cylinder base will be tested for movement 100 time-steps before being fixed. A sphere can fail to move vertically, but successfully move horizontally 1000 time-steps before it becomes fixed. If instead, it is desired that a sphere "stick" to the base of the cylinder upon contact, we would simply set *FSBO* to the critical fix value. Higher values for *FSI* and *FSHO* will cause spheres to fix faster and may lead to lower overall porosity values for the simulation, whereas lower values may lead to higher porosity values, but requires additional computational time.

The reduction of calculations needed for the simulation is at least the number of fixed spheres divided by the total number of spheres. So if 50% of the spheres are fixed, we would have at least a 50% reduction in calculations. The reduction may be more as the spheres which are candidates for being fixed have fewer movement options, so are on average more expensive to move as shown in Table 3.4. This may come at a cost of authenticity, as not all particles may actually stop, but their continued calculation is deemed irrelevant to the simulation results and computationally expensive.

Furthermore, the simulation can utilize the fixed-ness of spheres to determine when further sphere additions and movement has no or a limited effect on the results. From a practical point of view, we must consider that spheres will generally remain in their locality so that the cylinder will be packed and the simulation can be determined as complete.

3.5.3 Detecting Simulation End

The original simulation presented at WMSCI required user interaction to determine when the cylinder was packed. This is generally sufficient when only a few simulations are run that each take only a short amount of time. There are many options for detecting when a cylinder is packed, and the simulation should end.

The simulation end may be determined by (in no particular order) the following:

- 1) User interacts to indicate simulation termination
- 2) Porosity reduction value converges to a value. Specifically, the change in porosity reduction over a constant number of time-steps does not increase more than a given constant
- 3) Simulation is set to run a given number of time-steps, and simply stops when they have been executed. This is equivalent to simulating the EN process for a set amount of time
- 4) No new spheres have been introduced in a fixed number of time-steps
- 5) No spheres currently in the cylinder are capable of movement

The current simulation determines when the simulation is complete given a combination of conditions 4 and 5. This is utilized as the computation required is less than that of condition 2. First, we test condition 5 which can be tested when attempting

to move spheres in a time-step at limited additional cost. At this point, as per condition 4, an attempt to add new spheres should be tested before ending the simulation. If no spheres are able to be added, then the simulation is deemed complete and displays the results. Condition 4 also takes limited overhead as introducing spheres to the cylinder is already necessary for each time-step. On the other hand, condition requires that the porosity of the cylinder to be recalculated each step, which is not calculated in this version of the simulation.

3.6 Broadphase

The broadphase collision detection of the simulation is a component of collision detection that determines which particles should be considered for narrowphase collision described in Sections 3.4.4 and 3.4.5. We have implemented two algorithms, COI and sectoring, that have reduced the asymptotic complexity of each time-step by reducing the number of comparisons necessary in the broadphase. Each algorithm will utilize a subset of spheres that contain all the spheres that can potentially collide during a sphere's movement. There are various names given to this subset depending on the particular strategy used to generate it, we will cover this in more detail for each subsection. In general, we will call this set the broadphase collision set (BCS). The COI and sectoring methods have improved performance over the brute force method due to generating a smaller BCS of spheres for comparison thus reducing the number of sphere comparisons needed in order to move a sphere. This set may still contain spheres that can not cause a collision under any condition, but the goal should be to include the fewest number of spheres while containing all spheres that cause a collision in a time efficient manner. The

broadphase for collision detection is utilized for both sphere introduction of Section 3 4 6 and sphere movement of Section 3 4 7

3.6.1 Brute Force

The term *brute force* is applied to any method in which an exhaustive number of operations are performed. It implies that there is a more efficient manner of solving the same problem without performing every operation available. For example, when one searches for a word in the dictionary, if they viewed every single word starting at the first page until they found what they were looking for, they would be employing a brute force search. The advantages of brute force methods lie in simplicity, ease of implementation, and the guarantee that a solution will be discovered if it exists (since all possibilities are considered). Unfortunately, the brute force method is often inefficient in terms of time.

The original WMSCI paper presented results obtained from a brute force method. We compare these results to sectoring later in Section 4 3. The brute force method stores spheres in a linked list data structure. All spheres are contained within the single structure, therefore, each sphere must allocate memory to store its own size. The order of the spheres in the list are completely dependent on the order in which they are added to the list. The size and position of each sphere is irrelevant. Figure 3 8 illustrates the structure.

The third sphere shown in Figure 3 8 is in the head node of the linked list, and the first sphere is in the tail node. Spheres will be evaluated from the head of the list to the tail. Therefore, spheres are evaluated in the opposite order from which they were introduced. For the brute force method, the broadphase collision set (BCS) is the entire

linked list Psuedocode for the broad phase collision detection of the brute force method is displayed in Table 3 5

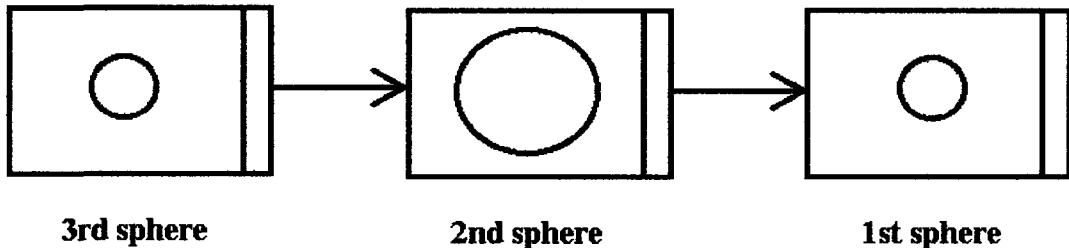


Figure 3 8 Brute force linked list representation

Table 3 5 Brute force broadphase collision detection

A1 Given a sphere A_N

A2 For each sphere B in the cylinder C, test for a collision between A_N and B

2 1 If a collision occurs according to Section 3 4 5, then return true

A3 Return false

For any sphere A_N that is generated either through particle introduction or movement of a particle A, we must test for collisions with every other sphere. In the worst case scenario, where A does not collide with any other sphere, we must make $N-1$ comparisons for a complexity of $O(N)$. Even if sphere A will collide with other spheres, it is likely that the number of spheres that would cause a collision are quite small compared to the total number of spheres. Further analysis will be carried out in Chapter 4. An advantage of this method is that it is trivial to add spheres of various sizes and to move all spheres regardless of size at the same time.

3.6.2 Cylinder of Influence (COI) Method

The COI method is categorized as a sort and sweep method [50]. It is based on a collection of sorted linked lists of spheres as shown in Figure 3.9. There is one linked list for each sphere size. We refer to each linked list as a sphereQueue Q . Each of these linked lists only hold spheres of a given size and each sphere of that size is stored in its corresponding sphere queue. In the figure, spheres of sizes 5, 15 and 20 nm are stored. We can denote a particular sphere queue Q_D with a subscript to indicate the diameter of sphere it contains. For example, Figure 3.9 contains Q_5 , Q_{15} and Q_{25} .

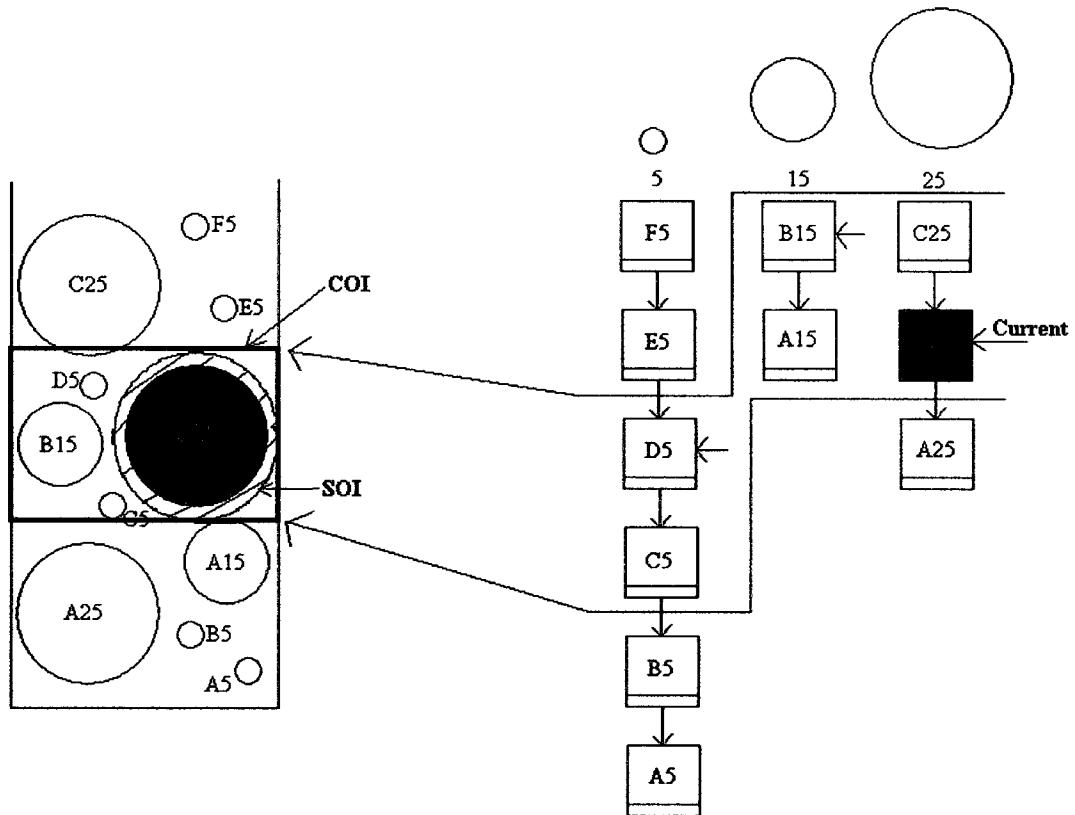


Figure 3.9 COI data structure and matching packed cylinder

As a side effect of this data structure change, the memory required to store each sphere is reduced. Assuming that the sphere size is stored as a double to allow for the possibility of chloride ions at approximately 0.66 nm, we save eight bytes per sphere compared to the brute force method with no negative effects. If there are a million spheres in a given simulation then we save 8 million bytes of RAM when running the simulation or approximately 7.6 MB.

Each sphere queue is sorted by y value. Recall from Section 3.3.4 that the top of the cylinder is set at $(0, 0, 0)$ with a y value of zero, and y value increases moving towards the base of the cylinder. The order of spheres in the sphere queues on the right side of Figure 3.9 correspond to the spheres depicted in the cylinder in the same figure on the left hand side. For sphere A_5 and sphere B_5 , sphere A_5 appears closer to the tail of the linked list and closer to the base of the cylinder because $A_{5y} > B_{5y}$.

When moving a sphere or inserting a sphere, we generate the broadphase collision set (BCS) first. In the COI method, there are two steps to this process. We have two subsets that are generated: the Cylinder of Influence (COI) and the Sphere of Influence (SOI). In Figure 3.9, the COI is represented by the darkened rectangle over the cylinder and represents a cylindrical cross-section, the SOI is represented by the shaded circle surrounding B_{25} and represents a spherical area. We will use these terms to refer to both the subset of spheres with which they intersect as well as the area they represent.

A sphere needs only check collisions against spheres that intersect with its SOI. We can easily test a sphere for intersection with the SOI as explained in Section 3.4.5 given that both are spheres. The radius of the SOI of A is determined by the sphere's range of movement denoted by the arrows as shown in Figure 3.10. The SOI is denoted

by the light dashed circular line while the COI is denoted by the bold dashed horizontal line. As the sphere is not allowed to move in the negative y direction, in practice, we reduce the top of the COI to reflect this fact and take the intersection of the SOI and the COI as the BCS.

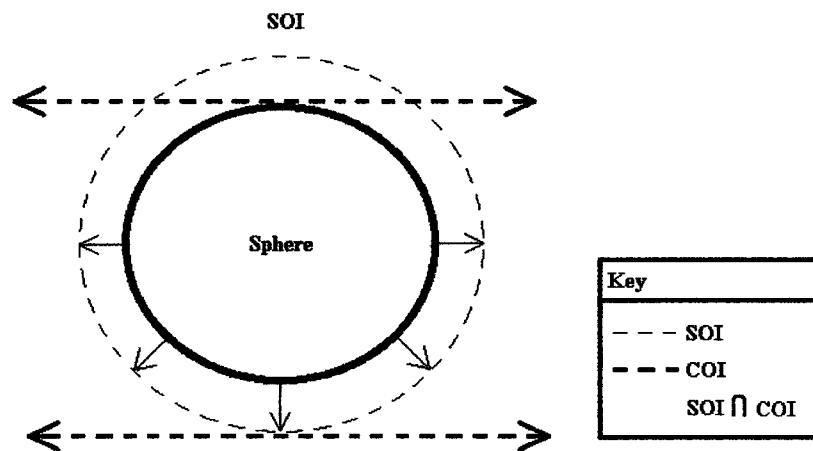


Figure 3.10 SOI and COI boundary

To generate the SOI is an $O(N)$ operation by the obvious brute force method of checking each sphere for an intersection with the SOI. Instead, we can reduce the number of comparisons by only considering spheres that intersect with the COI. The height of COI is exactly the diameter of the sphere moving plus the distance that can be moved with the top of the COI congruent with the top of the related sphere. For example, spheres of diameter 20 nm with a movement of 0.1 nm movement require a COI of height 20.1 nm and 2 nm spheres at the same movement rate require a COI of height 2.1 nm. Spheres that are within their radius of the COI are considered to be within the COI. A sphere S is considered to intersect with the COI of sphere A if it satisfies either Equation 39 or 40.

$$S_y \leq A_y \text{ and } S_y + S_R > (A_y - A_R) \quad (39)$$

$$S_y > A_y \text{ and } S_y - S_R < (A_y + A_R + A_M) \quad (40)$$

Recall that spheres are sorted by y values in sphere queues segregated by sphere diameter. During a time-step, we evaluate spheres in descending order of their y values, that is, from the front of the queue to the rear of the queue. Spheres can only move towards the front of each queue, thus no sphere will be evaluated more than once per time-step. In order to keep track of the next sphere in each sphere queue, we utilize a pointer to the next sphere to be processed in each queue. We will refer to this as the current pointer as illustrated in Figure 3.9. The next sphere to be evaluated will always be the sphere with the largest y value chosen only from current pointers. In our implementation, we only allow one sphere size to be moving at any given point in time, but the comparisons of sphere y values is still processed to maintain accurate current pointers. When a sphere is processed, the current pointer is moved towards the rear of its list.

The advantage of maintaining current pointers is that it improves the speed of determining which spheres intersect with the COI. Consider that we are processing a sphere A in Q. We must consider other spheres in Q for intersection with the COI. A_y is roughly at the center of the COI of A, thus there may be spheres above and below A in Q that also fall within the COI of A. We perform two linear searches of Q, one from A towards the front of the queue (base of the cylinder) using Equation 40 and one from A towards the rear of the queue (top of the cylinder) using Equation 39. For both searches, the algorithm stops when it encounters a sphere F that does not intersect the COI of A. All other spheres past these points cannot possibly intersect the COI of A as their y values

are even further away than F_y . We perform a similar search for each sphere queue. The search space for each queue varies based on the size of their spheres as shown in Figure 3.11.

Although the search spaces are larger for queues of spheres with larger diameters, each sphere is also larger, so there are not necessarily more larger spheres to search than smaller spheres. In fact, more small spheres could be placed within the search space of Q_1 than larger spheres in the search space of Q_9 .

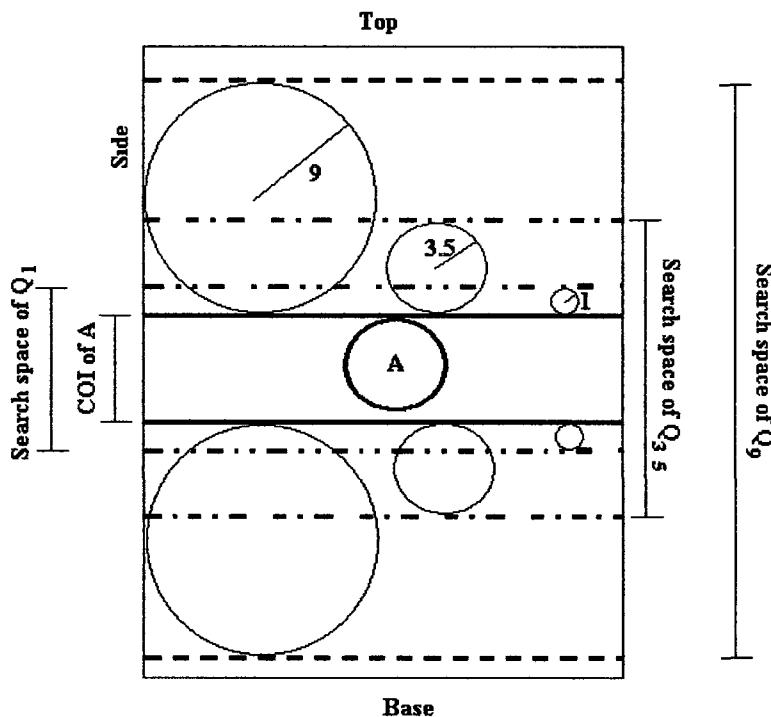


Figure 3.11 Search space of various queues in COI

The complete pseudocode for the broadphase collision detection using the COI method can be found in Table 3.6. The current sphere queue is searched first starting at the current sphere being tested for intersection. The other queues are then checked starting from their current sphere pointers. The COI broadphase collision detection will

return true if a collision is detected and false otherwise to the general psuedocode algorithm of Table 3 3

Table 3 6 COI broadphase collision detection

A1	Given a sphere A, set Q to the sphere queue such that $Q_D = A_D$
A2	For each sphere B in Q in the negative y direction where $B_y > A_y + A_R$
2 1	If a collision occurs according to Section 3 4 5, then return true
A3	For each sphere B in Q in the positive y direction where $B_y < A_y + A_R + A_M$
3 1	If a collision occurs according to Section 3 4 5, then return true
A4	If there is an untested sphere queue, set Q to that queue and go to A2
A5	Return false

3.6.3 Sectoring Method

This method is classified as a hierarchical grid method [50] In this method, the number of sphere comparisons is reduced compared to that of the COI method for larger cylinder sizes For simplicity, we will describe the method when packing spheres of identical diameters first Given a sphere S with diameter S_D , we divide the three dimensional space into cubes we refer to as sectors with sides of at least length $L = S_D$ as shown in Figure 3 12 This sector boundary repeats to create a mesh we refer to as the sector grid that overlays any finite space in which spheres are packed In other words, we inscribe a 3 dimensional object inside of a sector grid In the case of the cylinder, it cannot be evenly divided into cubes, thus there are sectors that are partially and completely outside of the cylinder but most sectors will intersect within the cylinder For

the sake of computational efficiency, we have an extra layer of sectors on the outside of the grid that are guaranteed to be empty as shown in Figure 3 13

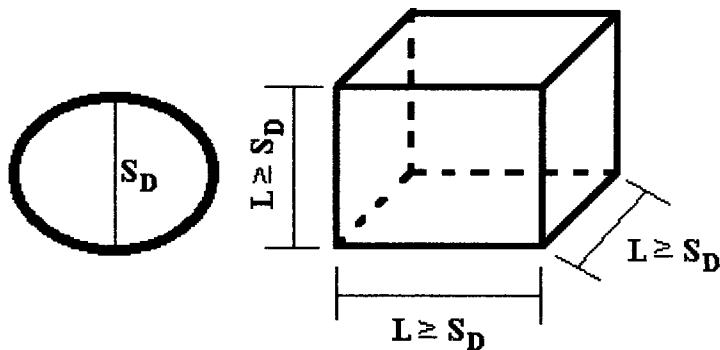


Figure 3 12 Sector length compared to sphere diameter

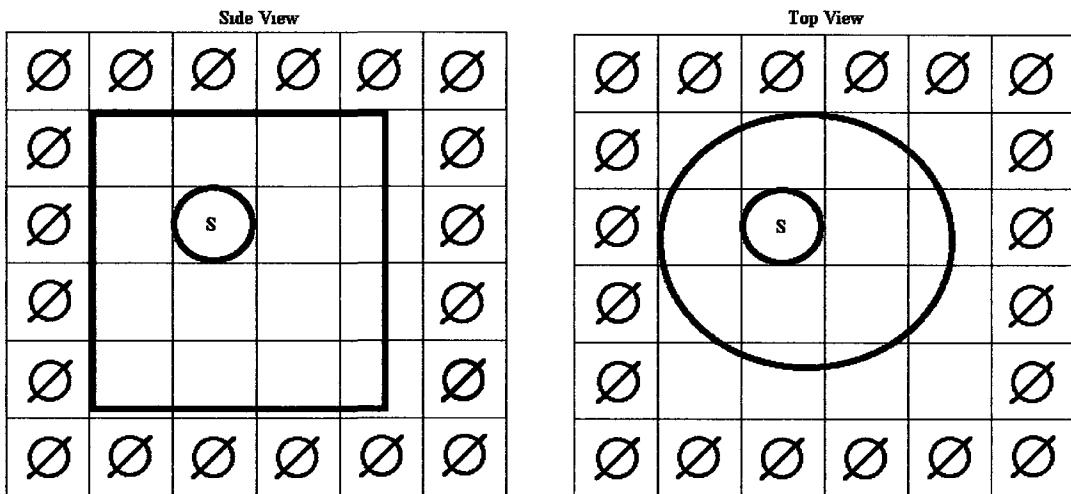


Figure 3 13 Sector grid in relation to a cylinder with empty sector padding

Each sector is uniquely identified by a three non-negative integer code (i, j, k) where i , j , and k are integers just like a typical three-dimensional array. We will refer to (i, j, k) as the sector code where i relates to the x-axis, j relates to the y-axis and k relates to the z-axis as shown in Figure 3 14. In Figure 3 14, Sector A would be coded as $(1, 3, 1)$, sector B would be coded as $(3, 3, 3)$ and sector C would be $(2, 1, 3)$.

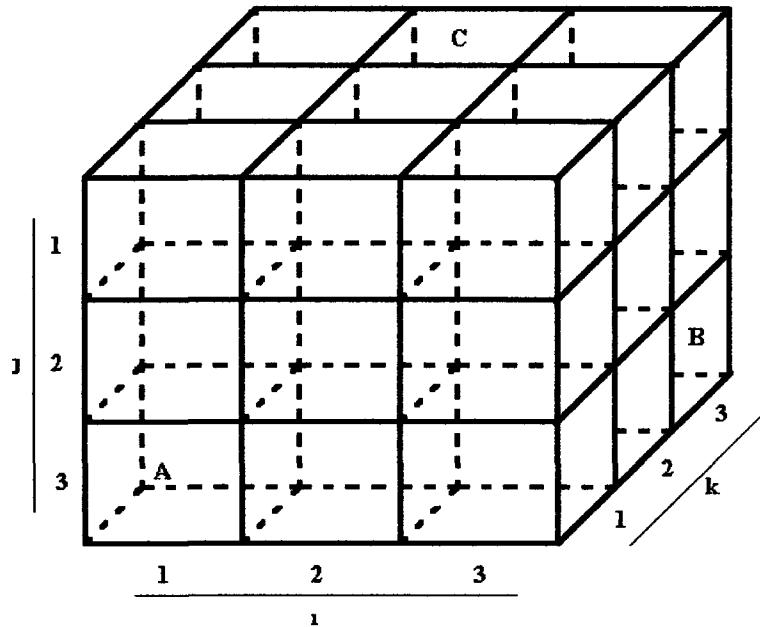


Figure 3.14 Sector addressing relationship to axes

Each sector maintains a list of spheres, so multiple spheres may be included in a sector. We can determine the sector code of the sector that contains a sphere S given that sphere's co-ordinates (S_x, S_y, S_z). This is achieved with Equations 41, 42, and 43. If the sphere center lies on a boundary of two sectors, it is only considered as a member of one sector as described by the Equations 41, 42, and 43.

$$i = \left\lfloor \frac{S_x}{sectorSize} \right\rfloor + 1 \quad (41)$$

$$j = \left\lfloor \frac{S_y}{sectorSize} \right\rfloor + 1 \quad (42)$$

$$k = \left\lfloor \frac{S_z}{sectorSize} \right\rfloor + 1 \quad (43)$$

The length of the sectors are determined by the sphere sizes and not the cylinder. Thus as the cylinder increases in size, more sectors will be used rather than larger sectors.

Let I, J and K represent the maximum values of i, j and k respectively. We can determine I, J and K according to Equations 44 and 45

$$I=K=\left\lceil \frac{C_D}{L} \right\rceil +2 \quad (44)$$

$$J=\left\lceil \frac{C_H}{L} \right\rceil +2 \quad (45)$$

For a grid G , we will refer to a sector as $G_{i,j,k}$ with the i, j, k code used as a subscript. For convenience we also define the neighbors of a Sector $G_{i,j,k}$. The neighbors of sector $G_{i,j,k}$ are all of the sectors which share a boundary with sector $G_{i,j,k}$, even if it is only a single point (which is the case for sectors diagonal to $G_{i,j,k}$). We can refer to the neighbors of G by indicating the difference in i, j, k code. For example, the sector directly in the positive x direction from G would be referred to as $G_{i+1,j,k}$. There are 26 neighbors of G , eight of which are horizontal, nine of which are above (in the negative y direction), and nine of which are below (in the positive y direction). We list the neighbors of G exhaustively by code in Table 3.7.

Table 3.7 Sector G and its neighbors by sector code

Horizontal	Above	Below
$G_{i,j,k+1}$	$G_{i,j+1,k+1}$	$G_{i-1,j+1,k+1}$
$G_{i,j,k}$	$G_{i-1,j-1,k}$	$G_{i-1,j+1,k}$
$G_{i-1,j,k+1}$	$G_{i-1,j-1,k+1}$	$G_{i-1,j+1,k+1}$
$G_{i,j,k-1}$	$G_{i,j-1,k-1}$	$G_{i,j+1,k-1}$
$G_{i,j,k}$	$G_{i,j-1,k}$	$G_{i,j+1,k}$
$G_{i,j,k+1}$	$G_{i,j-1,k+1}$	$G_{i,j+1,k+1}$
$G_{i+1,j,k-1}$	$G_{i+1,j-1,k-1}$	$G_{i+1,j+1,k-1}$
$G_{i+1,j,k}$	$G_{i+1,j-1,k}$	$G_{i+1,j+1,k}$
$G_{i+1,j,k+1}$	$G_{i+1,j-1,k+1}$	$G_{i+1,j+1,k+1}$

Sector length should be chosen carefully so that only neighboring sectors will need to be checked for collisions. Thus the search space for collisions remains constant regardless of cylinder size. Depending on the sector length chosen relative to sphere diameter, the neighboring sectors that must be searched can vary. We will present two variations that have been implemented.

First, it is important to note, that regardless of how large of a sector length is chosen, a sphere may always intersect neighboring sectors. To illustrate this, assume that a sphere S is at the corner of a sector that extends indefinitely. This sphere will be positioned such that if it were to be moved in the negative y direction or in the positive x direction, it would enter another sector as shown in Figure 3.15A. Such a sphere will intersect with neighboring sectors. Furthermore, even if a sphere S is completely contained in a sector, that is no part of the sphere extends into a neighboring sector, it can still intersect with spheres from neighboring sectors as they may extend into the sector of S as illustrated in Figure 3.15B. However, L can be chosen so that it is impossible for spheres of non-neighboring sectors to intersect with S as shown in Figure 3.15C where the dark rectangular box marks the furthest range of S as well as spheres of non-neighboring spheres. In order for this to be the case, $L \geq S_D$ must be satisfied.

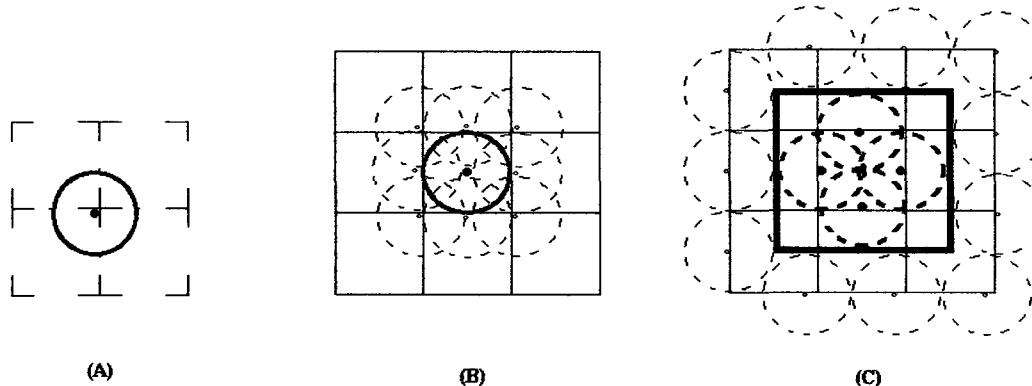


Figure 3.15 Sphere interactions with neighboring sectors

Proof 1

- 1) A sphere S may only extend at most S_R into a neighboring sector
- 2) Assume that two spheres of equal diameter exist with minimal distance between their sphere centers while being separated by a sector
- 3) In the optimal case, both spheres extend S_R into the shared sector for a total distance of S_D . These spheres may touch, but do not intersect as defined in Section 3.4.5
- 4) If L is chosen any smaller, then the spheres may intersect, thus $L \geq S_D$ must be satisfied to ensure that a sphere S may only intersect with spheres in its own sector and its neighbors

Given the conditions explained so far, for a sphere S in sector G , we can simply search G and its neighbors for possible sphere collisions. There is no SOI utilized in this method, instead our BCS is composed of the sectors mentioned. Although this approach was utilized in earlier implementations, an alternative version is currently in use. In the alternative version, we set L to twice the diameter of S as shown in Figure 3.16.

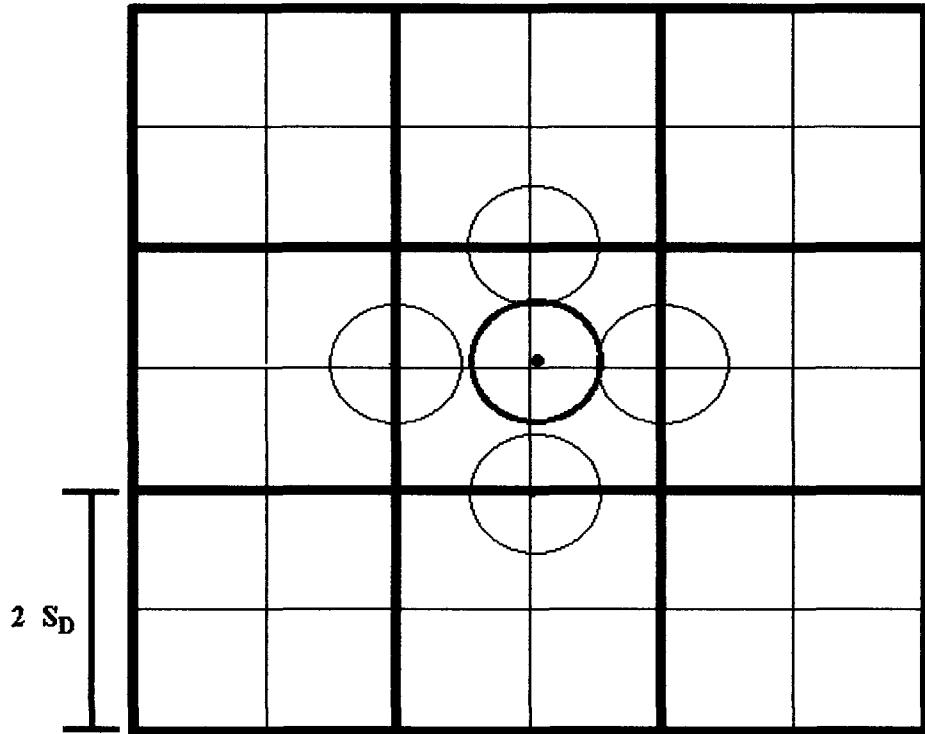


Figure 3.16 Two-dimensional representation of improved sectoring method

In this implementation, we can reduce the number of sectors to be searched to only eight. The shaded sectors in the figure may contain spheres that intersect with S and must be searched. The remaining four sectors that must be searched will all either be either directly below or above the shaded sectors. We determine which sectors must be searched by the octant of G in which S can be found (displayed as a quadrant in the figure). As shown in Proof 1, given that each octant has length S_D , S will be unable to intersect any sphere that is not in a neighboring octant.

The simulation automatically chooses a sector length given the particles sizes chosen. Larger sizes decrease memory allocations for the sphere array, but generally increase computational time. Smaller sizes generally reduce the computational time, but increase the memory requirements. With sufficiently large sectors, the algorithm could

be changed so that in some cases, even fewer sectors would need to be searched, but that was not implemented in our simulation

As there are differently sized spheres being packed into a cylinder, we utilize a separate sector grid for each different sphere size. This is similar to the sphere queues of COI. In the same manner as sphere queues, each sphere grid only contains one sphere size and the size information is stored in the sector grid instead of within each sphere. The dimensions of each sphere grid do not have to be identical, in fact, the dimensions for each sphere grid will be a function of the cylinder parameters and sphere size it is associated with according to Equations 44 and 45. A two-dimensional example is shown in Figure 3.17. The larger sector grid is marked with bold lines while the smaller sector grid is marked with thinner lines. Note from the figure, that the sector grids do not align perfectly, the smaller sector grid is not contained within the larger sector, they simply represent sphere locations of different sizes in the same space. When moving a sphere S , we must test for collisions not only in the sphere grid of S , but also every other sphere grid that is present. When S is a larger sphere, we must search more than just the neighboring sectors. It is clear to see that the larger sphere of Figure 3.17 can be allocated to a smaller sector G , but can intersect with spheres from sectors other than the neighbors of G . We do not implement this functionality as the simulation packs and fixes all larger spheres first. As a result, any mobile sphere will be smaller than sphere grids utilized, thus Proof 1 is satisfied and only neighboring sectors will need to be searched.

For efficiency, we also maintain separate linked lists of spheres similar to the COI method. We maintain separate lists for fixed and unfixed spheres. There is also a separate list for each sphere size. When evaluating spheres for movement, we evaluate

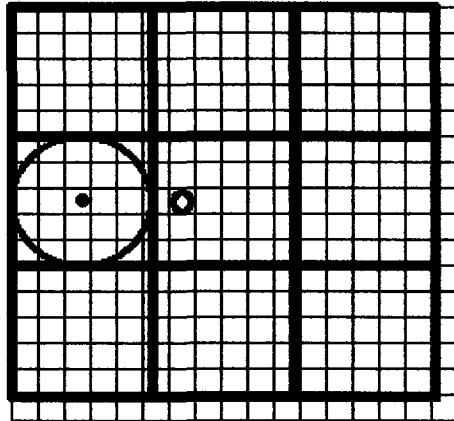


Figure 3.17 Sector grid overlays

spheres in the unfixed list of the current sphere size being packed. We also utilize these lists for the graphical rendering of spheres. An alternative approach would be to iterate through each sector, but this approach may reduce performance in cases where many sectors are empty. For example, at the simulation start, the cylinder is mostly empty, thus many sectors would be evaluated unnecessarily.

The complete pseudocode for the broadphase collision detection using the sectoring method can be found in Table 3.8. The current grid is searched first starting at the current sector of the sphere being tested for intersection. Neighboring sectors are then checked. If no intersection occurs, the process is repeated for other sector grids. The brute force collision detection will return true if a collision is detected and false otherwise to the general pseudocode algorithm of Table 3.3.

Table 3 8 Brute force broadphase collision detection

-
- A1 Given a sphere A, set G to the sector grid such that $L = A_D$
 - A2 Determine the Sector $G_{i,j,k}$ in which A is contained
 - A3 For each sphere B in $G_{i,j,k}$, test for intersection between B and A
 - 3 1 If a collision occurs according to Section 3 4 5, then return true
 - A4 Create a subset of neighbors of $G_{i,j,k}$ according to the position of A
 - 4 1 For each neighbor in the subset
 - 4 1 1 For each sphere B in G, test for intersection between B and A
 - 4 1 1 1 If a collision occurs according to Section 3 4 5, then return true
 - A5 If there is an untested sector grid, set G to that grid and go to A2
 - A6 Return false
-

CHAPTER 4

SIMULATION RESULTS AND ANALYSIS

In this chapter, we discuss the simulation results and analyze the brute force, cylinder of influence (COI) and sectoring methods for time and porosity reduction. The statistical standard of referring to all graphical representations of the data as plots will be used. We will present plots of the COI and sectoring method results, perform regression analysis of said results, compare our results to other packing method results, compare the results to data obtained in physical experimentation and perform an asymptotic complexity and time analysis.

4.1 Sectoring And COI Results

In this section we will present the results of the simulation work for the COI and sectoring methods. We will present various plots obtained from simulation work. Results for the porosity reduction of the COI method can be seen in Figure 4.1. These results are based on packing 2 and 20 nm particles into cylinders of various sizes at a movement rate of 0.5 nm per time-step. Cylinder diameter varies from 10 to 50 nm in 4 nm increments. Height varies from 50 nm to 500 nm in 50 nm increments. The large 20 nm particles cannot pack into the cylinders smaller than 2 nm. The change in porosity is clearly visible in Figure 4.1. Porosity peaks at the 22 nm diameter cylinder where the 20 nm particle fits closely to the cylinder. Porosity reductions drops and rises in a parabolic

fashion. The effect is more noticeable as cylinder height increases. This may be due to a the parameters chosen for the simulation, but it may imply that smaller spheres can become stuck when introduced into a cylinder packed with larger spheres. The COI method gives porosity reduction anywhere from 0.35 to 0.65 depending on the conditions.

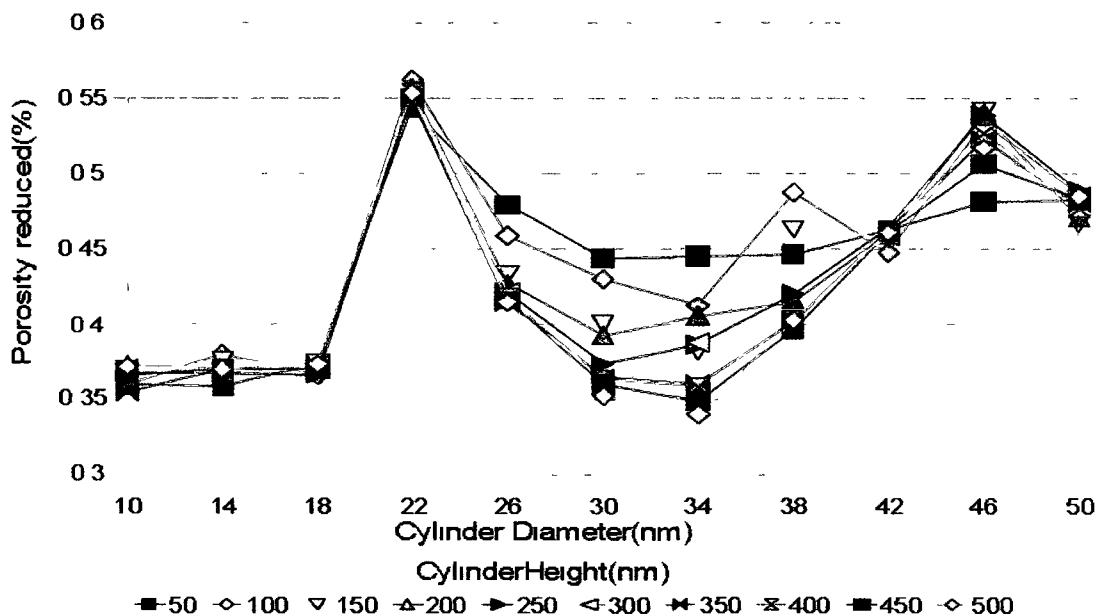


Figure 4.1 COI porosity reduction for 2 nm and 20 nm spheres at 0.05 movement

We ran similar simulations utilizing the sectoring method. The results can be seen in Figure 4.2. The sectoring method seems to achieve higher porosity reduction values of 0.41 to 0.65, but this may be attributable to different parameters for the fixing of spheres. A drop of porosity values is still observed but not for all cylinder heights, and not to the same degree. More random trials may be necessary to investigate this phenomena.

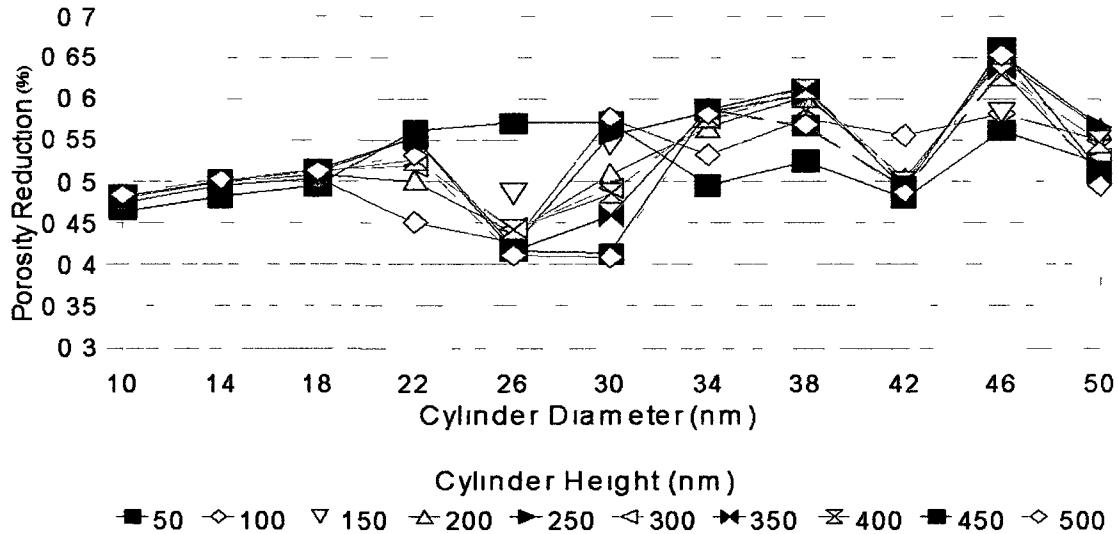


Figure 4.2 Sectoring porosity reduction for 2 and 20 nm particles at 0.1 nm movement

We have also collected data for the numbers of spheres packed for each sphere size. Larger spheres pack in the COI method without issue as shown in Figure 4.3. The packing of 20 nm particles for sectoring is similar to COI as can be seen in Figure 4.4. Close observation reveals that Figure 4.3 and Figure 4.4 are nearly identical although they are generated using different algorithms. This is not surprising as each algorithm is designed to improve the speed of the simulation without affecting the outcome.

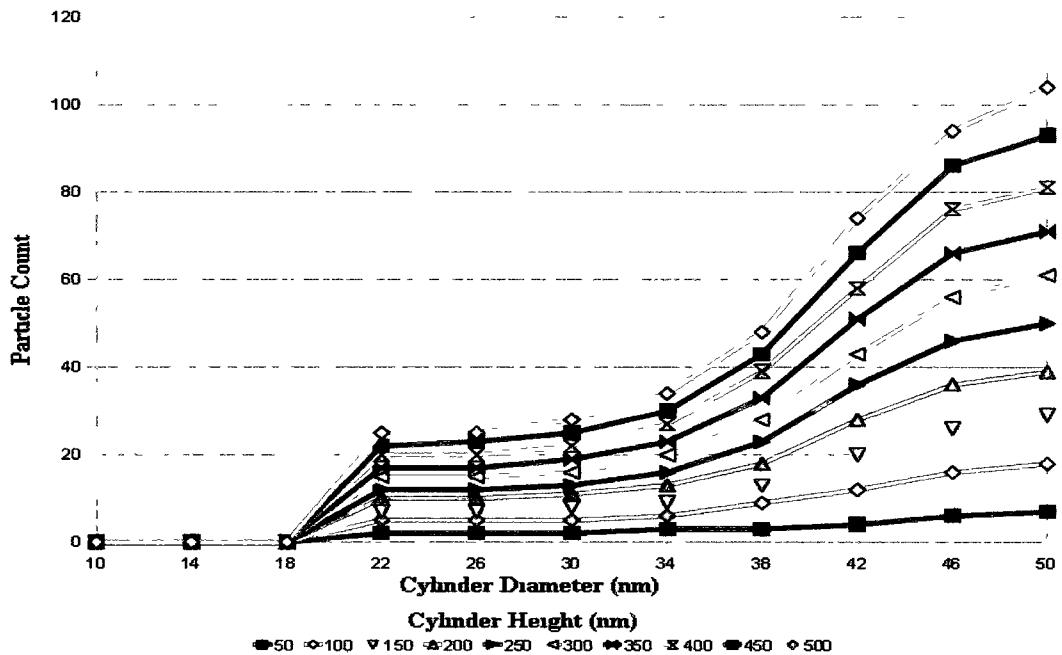


Figure 4.3 Counts of 20 nm particles packed with COI at various cylinder sizes

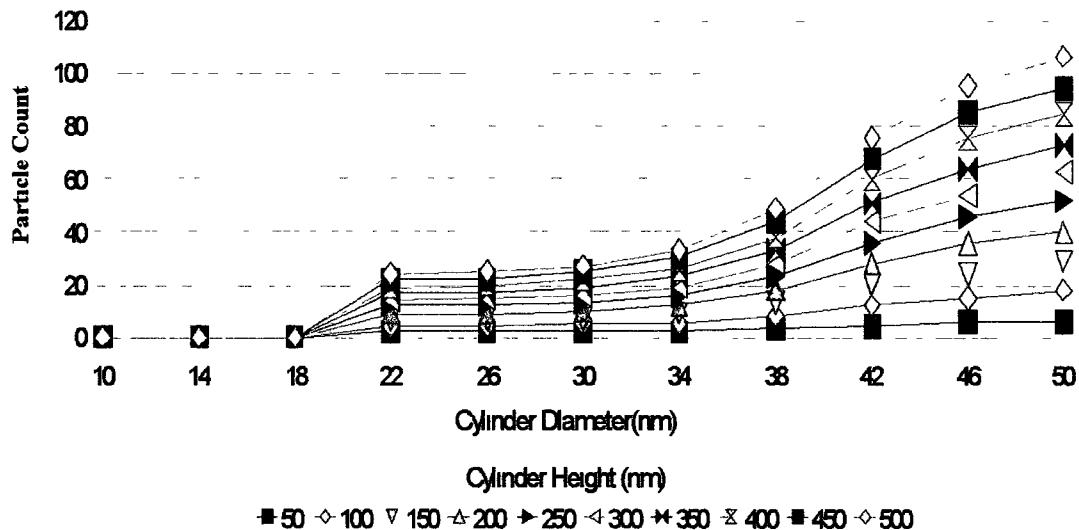


Figure 4.4 Counts of 20 nm particles packed using the sectoring method

It is also important to note that the important feature of packing is not absolute sphere size and cylinder size, but rather the ratio of sphere size to cylinder size. For example, packing 20 nm particles into a 500 nm height by 50 nm diameter cylinder is

congruent to packing 200 nm particles into a 5000 nm height by 500 nm diameter cylinder. Results will be identical if the same random seed is used regardless of the absolute sizes as long as the ratio between cylinder and particle size is identical. As a consequence, the simulation results can be used to predict the packing of larger cylinders using larger particles. Considering that concrete pores can be 10,000 nm in diameter, we can predict results of packing larger spheres into the cylinder as long as the ratios of sphere diameters to cylinder dimensions are congruent.

We conclude with an image of a packed cylinder generated by the sectoring method in Figure 4.5. There is clearly an unpacked area in the cylinder that accounts for the irregular porosity reduction presented in this section. Particles may aggregate in the cylinder and prevent other particles from passing. More details of this are presented in Section 4.4.

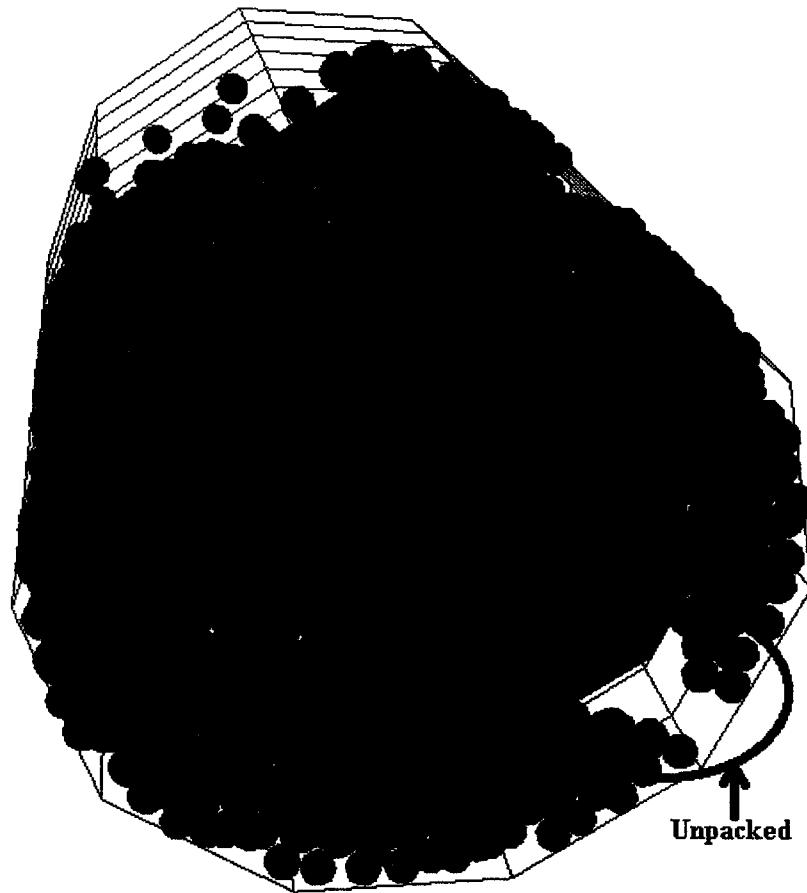


Figure 4 5 Graphical representation of a packed pore obtained from the implementation of the sectoring method

4.2 Linear Regression

The terminology and formulas used for regression analysis will follow [51] Regression analysis is used in this paper to generate formulas that attempt to describe porosity reduction values based on the independent variables of particle size, pore radius and pore height. A detailed description of the theory of linear regression can be found in appendix D. Figure 4 6 illustrates a scatter plot for 100 nm height cylinders of various diameters packed with 20 nm and 2 nm particles using the sectoring method. A regression line has been plotted with both linear and log terms. The blue dashed line is

the log transformed model as per Equation 46. Cylinder height is significant at $p < 0.001$ as is the model, but $R^2 = 0.53$ indicates that only 53% of the variance is explained. A better fit of $R^2 = 0.59$ was obtained with Equation 47, but that is to be expected with more terms. A graph of boxplots has also been generated in Figure 4.7 to illustrate the averages, variance and outliers. The graphs show that the variance decreases as the cylinder diameter increases.

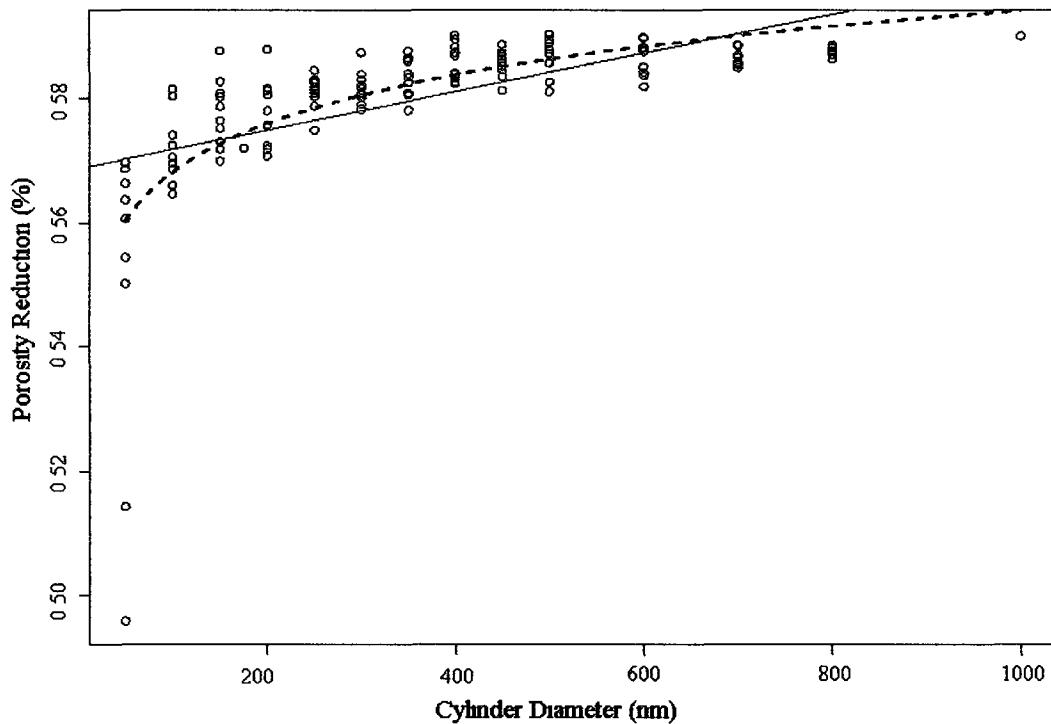


Figure 4.6 Scatterplot of 100 nm height cylinders packed with 2 and 20 nm spheres

$$PR = 0.5161 + 0.0113 \ln(C_D) \quad (46)$$

$$PR = 0.4757451 - 0.00003 C_D + 0.0207 \ln(C_D) \quad (47)$$

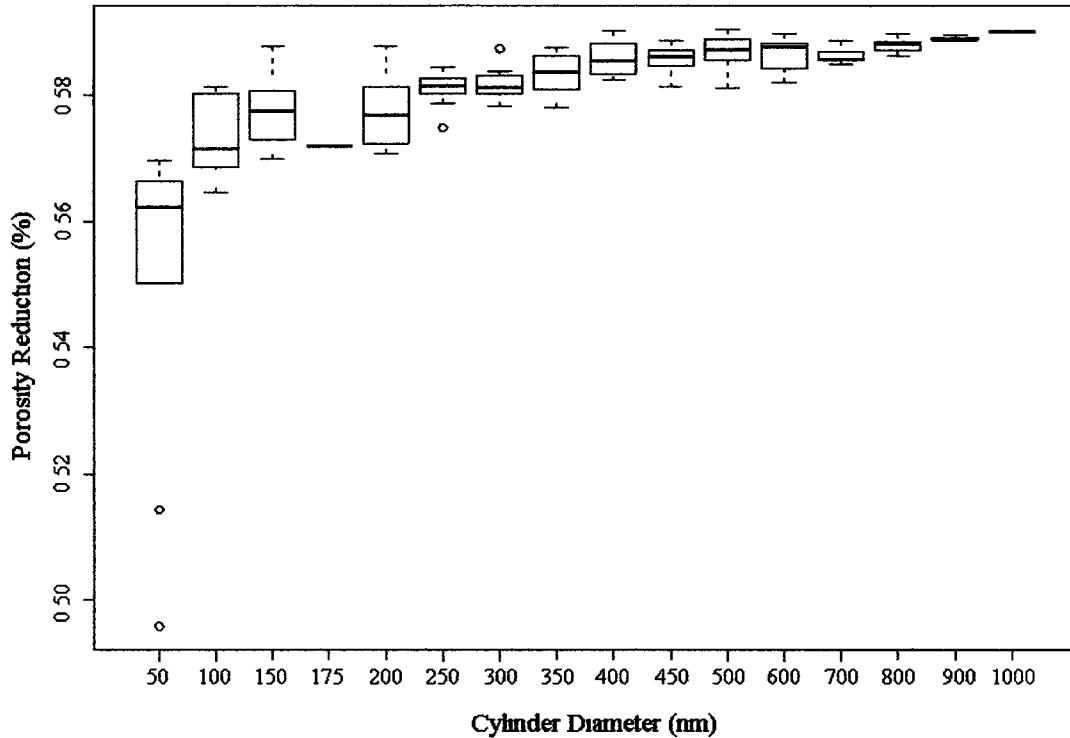


Figure 4 7 Boxplots of porosity reduction given cylinder diameter

A simple linear regression was also performed on 269 simulation runs stored in a MySQL database. The simple linear regression results are shown in Equation 48. All terms were significant at $p < 0.001$ except for cylinder diameter which was not significant ($p = 0.3$) at $\alpha = 0.05$. The model was also significant at $p < 0.001$ with a goodness of fit of $R^2 = 0.84$. Given the results of Equations 46 and 47, we also performed a log transform of C_D for the data set and repeated the regression to obtain Equation 49. In this model, all terms are significant at $p < 0.001$. The model is also significant at $p < 0.001$, but the goodness of fit does not greatly improve as $R^2 = 0.86$.

$$PR = 4678 - 0.0002 C_H + 0.0073 S_{1D} - 0.0055 S_{2D} \quad (48)$$

$$PR = 4441 + 0.0081 \ln(C_D) - 0.0003 C_H + 0.0066 S_{1D} - 0.0048 S_{2D} \quad (49)$$

We also perform a regression analysis of the WMSCI data presented in Section 4.3 with the resulting Equation 50. There are 10 random runs for each data point, thus 140 data points for this analysis. As all cylinders were 20 nm in height, height cannot be analyzed. All other terms were significant at $p < 0.001$. The model is significant at $p < 0.001$ with $R^2 = 0.935$.

$$PR = 425 + 0.0013 C_D + 0.0069 S_{1D} - 0.0078 S_{2D} \quad (50)$$

4.3 Comparison To Other Methods

We will compare results of our sectoring method to results presented at [3]. We followed the procedure of a single simulation run for expediency and calculated porosity reduction runs for the same parameters presented in the table. As shown in the table, for 20 nm diameter and height cylinders for various spheres sizes, the sectoring method generally obtains results that fall within those of the brute force implementation and the analytical method presented at [3]. The adjustment of the fixed score control constants as well as the movement rate of spheres may affect the final porosity values. The brute force implementation does not fix spheres and runs indefinitely until the user stops the program. As a result, it will achieve higher packing densities given sufficient time. Adjusting the general algorithm for sectoring could achieve similar results at a time cost. The table shows a need to investigate sectoring settings more closely and to consider alternative program termination strategies as covered in Section 3.5.3. On the other hand, Table 4.2 illustrates the increased processing capability of sectoring.

Table 4 1 Comparison of analytical, brute force and sectoring results for 20 nm height and diameter cylinders

Method	Particle Sizes in nm				
	2 & 10	2 & 8	2 & 4 & 6	2 & 6	2 & 4
Analytical	46 00%	43 00%	47 00%	45 00%	49 00%
Sectoring	51 10%	48 80%	47 50%	48 60%	47 10%
Brute Force	55 00%	53 00%	49 00%	51 00%	49 00%

Table 4 2 Comparison of analytical, brute force and sectoring results for 20 nm height and 50 nm diameter cylinders

Diameters of Particles S_1 & S_2	Source	Particle Counts $n(S_1) + n(S_2) = n(S)$	Porosity Reduction
2 & 20	Analytical	544+4=548	48%
	Sectoring	3502+2=3504	58 70%
2 & 16	Analytical	994+7=1001	49%
	Sectoring	3025+5=3030	59 60%
2 & 10	Analytical	1068+34=1102	57%
	Sectoring	1829+27=1856	55.50%
2 & 8	Analytical	2290+48=2338	57%
	Sectoring	1329+56=1385	52 40%
2 & 6	Analytical	1348+138=1486	54%
	Sectoring	845+143=988	50 20%
	Brute	852+156=1008	54.00%
2 & 6 7& 20	Analytical	272+8+4=284	49%
	Sectoring	817+93+2=912	56 80%
2 & 4 & 6	Analytical	1252+18+138=1408	55%
	Sectoring	379+48+143=570	49.30%
	Brute	414+62+152=628	54.00%
2 & 4	Analytical	720+455=1175	46%
	Sectoring	379+542=921	50 30%

It is important to note that many brute force results are missing from the table as the simulation results for the given parameters could not be completed in a reasonable time. The brute force implementation requirement for user interaction may have been a factor as well. We investigate the scalability of the brute force methods in relation to the COI and sectoring method in Section 4 5. The table illustrates the difference between the

analytical method which is a mathematical model based on manual packing that packs the optimal number of larger spheres first to the sectoring method which loosely packs larger spheres. In addition, the sectoring method simulates the flow of particles, which the analytical method cannot do. The simulation is generally better at packing larger number of smaller spheres accurately as each sphere is packed as opposed to the numbers being extrapolated.

4.4 Relationship To Experimental Results

The simulation results greatest porosity reduction achieved was approximately 65%. The greatest porosity reduction achieved among the empirical results was 60%. Experimental results typically achieved 50% reduction of porosity similar to the simulation results [3]. The simulation data stored in the database has a median of 0.5750 and a mean of 0.5504. The standard error is 0.0054 at $\alpha = 0.05$ for a 95% confidence interval of 0.5504 ± 0.0054 .

Each simulation run can determine the amount of porosity reduction for an individual pore of a fixed diameter and height when filled with particles of given diameter. On the other hand, many physical test results may only have recorded the porosity reduction for a section of concrete. Mercury intrusion porosimetry (MIP) has also been used to determine the aperture sizes of pores in the concrete before and after electrokinetic nanoparticle (EN) treatment. We will average our simulation results for comparison. Utilizing all porosity reduction in the database, we obtain an average porosity reduction of 55%, a minimum of 44% and a maximum of 65%. Previously obtained results from the sectoring method have a minimum porosity reduction of 41%

and the previously obtained results from the COI method have a minimum porosity reduction of 34% These results are shown in Figure 4 8

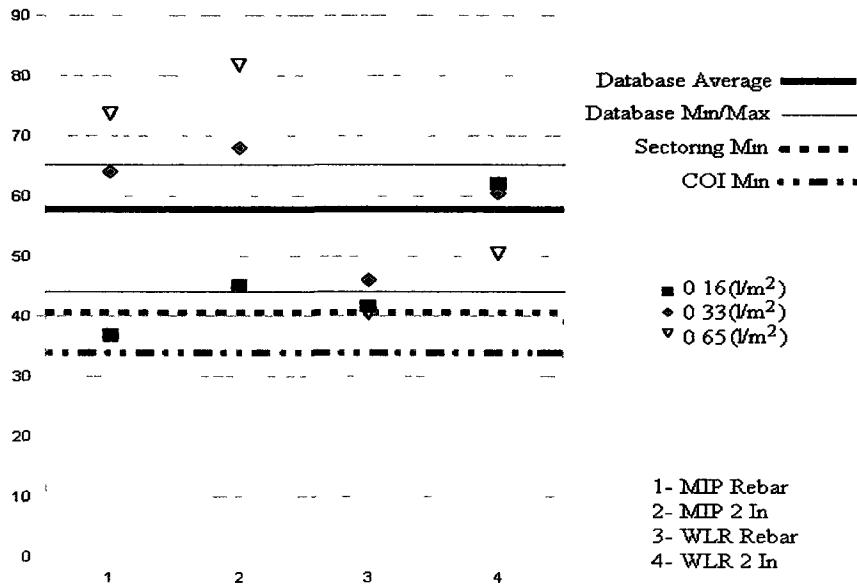


Figure 4 8 Comparison of physical results to simulation results

As shown in the figure, most data points fall within the same ranges as the simulations predict Some mercury intrusion porosimetry (MIP) measurements show higher porosity reduction values than predicted by the simulations, but this is to be expected as MIP is an inaccurate measurement tool for concrete porosity as described in Section 2 3 2 In the MIP data used for this analysis, no pores of diameter 10 or smaller were detected The amount of pressure needed to detect these pores is high and the MIP measurements undoubtedly is not accounting for those spaces The disagreement between the MIP and weight loss ratio (WLR) measurements further illustrate the inaccuracies involved in measuring concrete porosity

Despite the inconsistencies between the measurements obtained, a trend is clear between samples taken at the concrete-rebar interface and samples taken 2 inches away

from the rebar. In all data pairs, the porosity reduction is greater 2 inches away from the rebar as compared to the concrete-rebar interface. Taking horizontal cross-sections of a cylinder packed in the simulation yields similar results as seen in Figure 4.9.

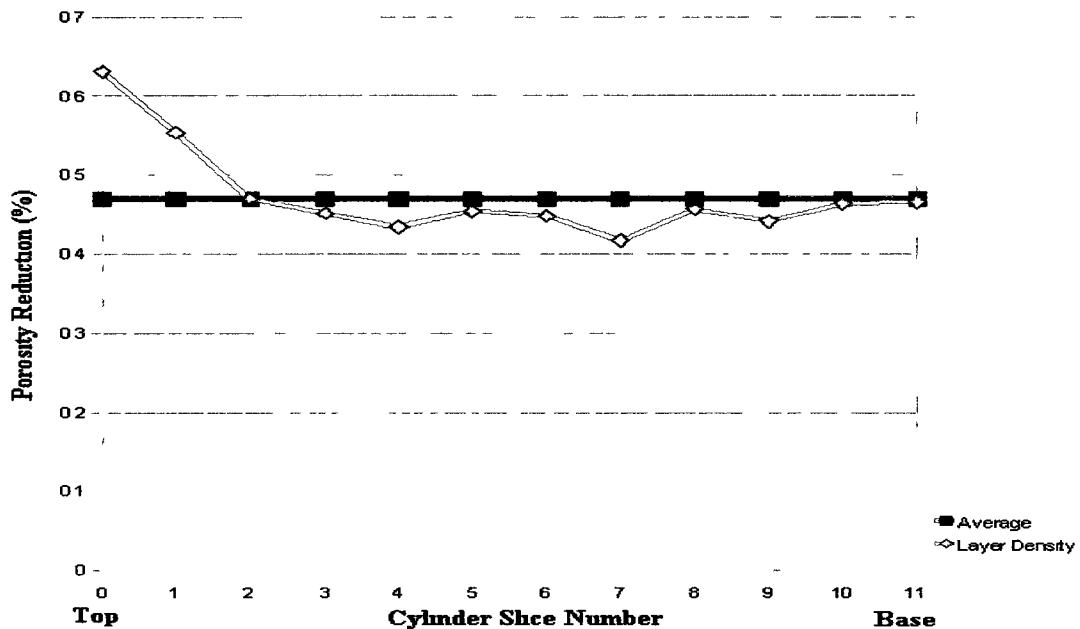


Figure 4.9 Cylindrical cross-section porosity reduction

The porosity is generally higher at the top of the cylinder and decreases towards the base of the cylinder. In the figure a 500 nm height and 65 nm diameter cylinder is divided into 11 equal cross-sections and the porosity reduction of each slice is calculated using the partial sphere volume equation of Section 3.3.3.

4.5 Time Analysis

All broadphase simulation methods work within the framework of the general simulation method. We will begin by analyzing the asymptotic complexity of the simulation in general without consideration of the broadphase (we will assume the broadphase completes in constant time). We will extensively utilize asymptotic

complexity notation as described in Section 3.4.2. Recall that spheres are introduced at the cylinder top and move towards the cylinder base. We will eventually pack n spheres into the cylinder. Each sphere will have to be moved on average M times until it becomes fixed. We cannot know M exactly as spheres can move horizontally, or diagonally down, but we expect M to be linear based on height. If we assume that a sphere S always moves directly towards the base then from the top of the cylinder, it will move approximately M_D times according to Equation 51

$$M_D = \frac{C_H}{S_M} \quad (51)$$

If we consider only diagonal downward movements then we would simply need to multiply by a constant greater than one. If we further assume that a sphere can move horizontally a constant number of times for each before being fixed, then we can again multiply by a constant greater than one to represent this fact. We combine both constants and represent them simply as c . We have an upper bound for movement represented by M_A in Equation 52

$$M_A = c \frac{C_H}{S_M} \text{ where } c \geq 1 \quad (52)$$

Although c is unknown, it is a constant and does not change the fact that M is directly related to C_H and indirectly related to S_M as shown in both Equations 51 and 52. As we will move n spheres in a worst case M times our simulation must perform approximately nM particle movements in the worst case. As shown earlier M is only affected by C_H and not cylinder diameter C_D . Also, the number of particles that can be packed increases linearly as C_H increases as illustrated in the plots of Figure 4.10

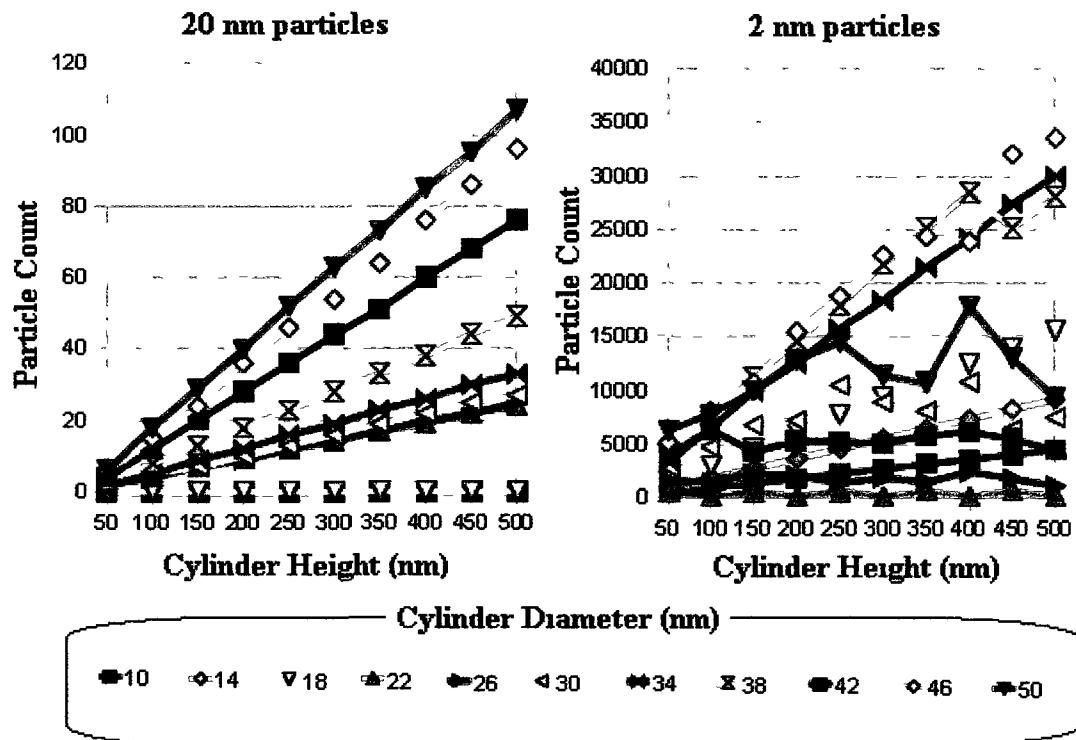


Figure 4 10 Sphere counts relationship to cylinder height and cylinder diameter

Note that when particles of a single size are packed into a cylinder, the relationship between particle number and cylinder height appears completely linear. When a smaller particle size is packed it does not always have a perfect linear relationship, but it clearly not of a higher order than linear. Therefore, if we set S_M and C_D to constant values and only increase C_H , then we will observe a linear increase in M and a linear increase in n , thus $n M$ has a complexity of $O(N^2)$ when increasing only cylinder height.

We also consider results obtained from the website regarding increases in cylinder diameter as illustrated in Figure 4 11 and Figure 4 12. In Figure 4 11, a plot generated by R shows the quadratic relationship between large packed particles as cylinder diameter is changed while all other factors are held constant at $C_H = 100$ nm, $S_{ID} = 20$ nm and $S_{2D} =$

2 nm. The dashed blue line is the fitted regression line fitted by R and written in Equation 53. All coefficients are significant at $p < 0.001$ and the equation has an R^2 value of one. Similarly, Figure 4.12 plots the number of smaller particles packed after the larger particles are packed. Again, we observe a quadratic relationship between the number of smaller particles and cylinder diameter. The fitted quadratic regression curve obtained using R is shown as the dashed blue line and written as Equation 54. In this case, all coefficients are significant with $p < 0.001$ and the equation has an R^2 value of 0.9994.

$$n(S_{ID}) = 0.0087 (C_D)^2 - 14.78 \quad (53)$$

$$n(S_{ID}) = 2.35 (C_D)^2 - 669.1 \quad (54)$$

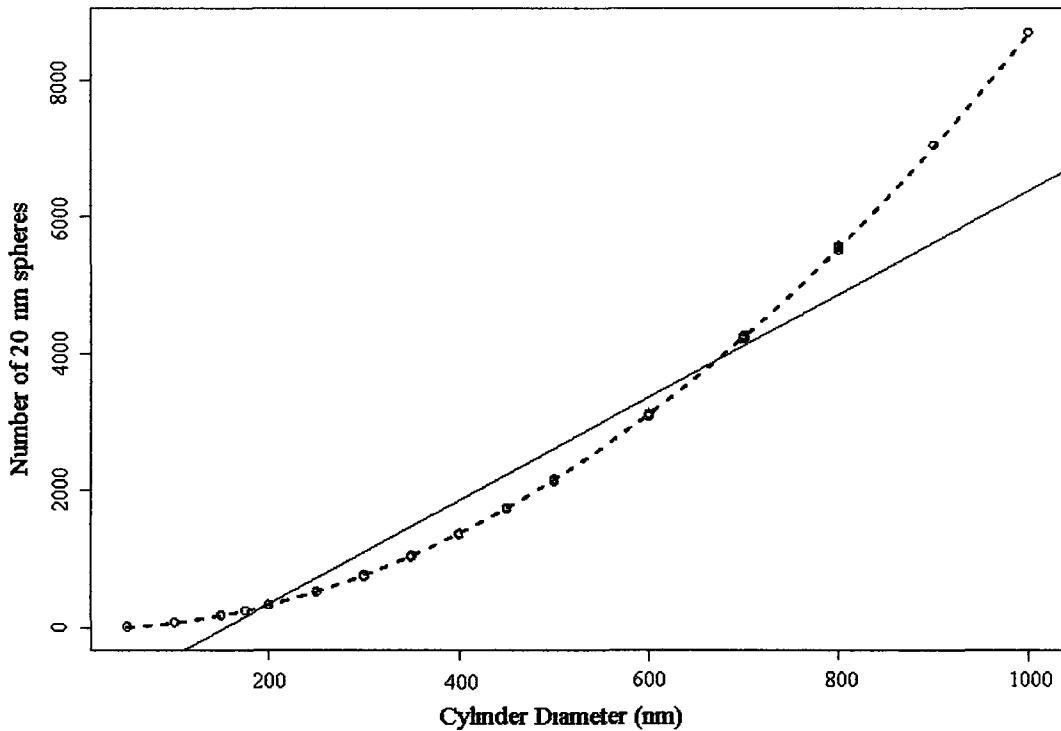


Figure 4.11 Plot of count of 20 nm spheres in relation to cylinder diameter

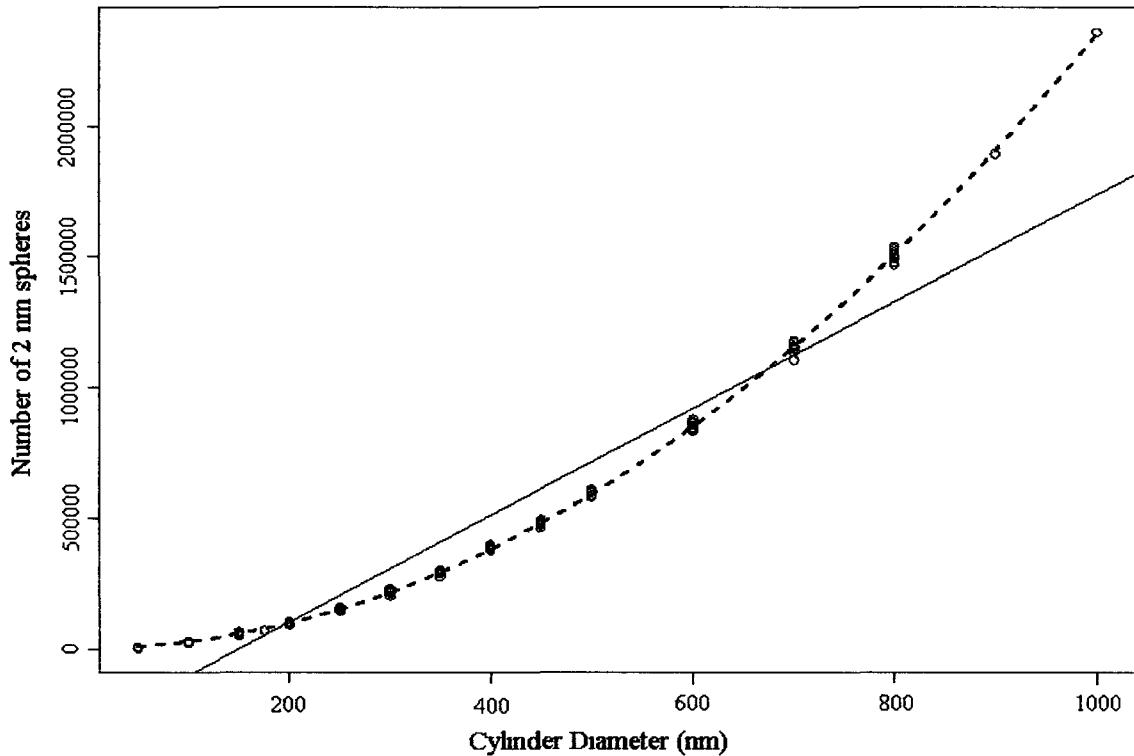


Figure 4.12 Plot of count of 10 nm spheres in relation to cylinder diameter

If we set S_M and C_H to constant values and only increase C_D , then we will observe no change in M and a quadratic increase in n , thus $n M$ has a complexity of $O(N^2)$ when increasing only cylinder diameter. We therefore observe a complexity of $O(N^2) O(N^2) = O(N^4)$ if both height and diameter are increased at the same rate, that is, if N is representative of a unit dimension C_U of the cylinder. Any algorithm that positions n spheres into a cylinder C of unit dimension C_U where $C_D = C_H = C_U$, will be at least $O(N^3)$. That is where spheres are positioned immediately in their final position in constant time. It may also be possible to reduce M to a constant if spheres flow, but are not required to start at the top of the cylinder.

In order to compare the efficiency of the brute force, COI and sectoring methods, we will present the asymptotic complexity for the broadphase of each algorithm. In particular, we will focus on the complexity of moving a single sphere S . The complexity is directly related to the number of spheres comparisons required to move S . For ease, we will base our analysis on the number of spheres n in the cylinder. Recall that n is directly related to cylinder size and can be estimated according to equation for some positive constant $c < 1$. This is simply the volume of the cylinder divided by the volume of each sphere. The constant c is equivalent to the packing density. Thus, even though we are taking N as the number of particles n in our assessment here, realize that n is cubically related to the cylinder dimensions.

$$n(S) = c \frac{\pi (C_R)^2 C_H}{\frac{4}{3} \pi (S_R)^3} \quad (55)$$

In the brute force method, all spheres are potentially compared to all other spheres on insert/move operations. For this analysis we will consider two scenarios: 1) A temporarily moved sphere S_N will not intersect with any other sphere in the cylinder and 2) S_N will intersect with one or more spheres in the cylinder. For the first case, if S_N will have no intersections, given that there are n spheres in a cylinder at any given time, we must make $n-1$ tests for each movement direction and the operation is $O(N)$. The algorithm is also $\Omega(N)$ as the algorithm must always exhaustively search the entire cylinder. Thus, the brute force method sphere movement is $\mathcal{O}(N)$ for any sphere that will not intersect any other sphere on a movement attempt. If S_N will intersect with another sphere B , then the collision could occur on the first time-step, thus the algorithm is also $\mathcal{O}(1)$. In the worst case scenario, the collisions would be tested last, and given M collisions, we must test $n-M$ sphere intersections. Clearly M should be considered as a

constant and the surface area of S_N is a constant, but the volume of the cylinder and thus n can be increased arbitrarily. In this case the algorithm is $O(N)$ and thus $o(N)$ when a sphere movement will result in collision. It is also valuable to note that the search space of the brute force is exactly the total volume of the cylinder.

We will analyze the COI method similarly based on the two scenarios given for the brute force method. In addition, we will consider the complexity according to whether the diameter is set to a constant value or not. This leads to a total of four scenarios. To start, we should consider the area to be searched for sphere collisions. According to the Area formula for a cylinder, $A = \pi r^2 h$ where r is the radius of the cylinder and h is the height of the cylinder, substituting for the COI as described in Section 3.6.2, we obtain Equation 56. The area A for the COI may be smaller if the COI is near the top or base of the cylinder. Recall that a sphere B outside of the COI can intersect with it, so the search space is larger than the COI itself. In the general case, when considering a sphere B intersecting the COI we must search a space with area A given by Equation 57.

$$A = \pi (C_R)^2 (S_D + S_M) \quad (56)$$

$$A = \pi (C_R)^2 (S_D + S_M + 2 B_R) \quad (57)$$

We created the COI method with the assumption that pores are long and narrow, thus height is a much more important consideration than diameter. It is important to note that the size of the COI does not increase as the pore height increases, thus the number of sphere comparisons is not affected by cylinder height increase. To prove this, assume that the diameter of a cylinder is fixed. Then the number of spheres that can be contained in a COI is a constant in regard to changes in cylinder height. As a result, we only have a

constant number of sphere comparisons when we move a sphere so the operation is $O(c)$ with a fixed pore diameter. This holds whether a collision will occur or not. It is possible that a collision could occur on the first step for a complexity of $\Omega(1)$, as one is a constant, we can consider these scenarios as $\Theta(c)$ in terms of complexity. Although moving a sphere requires that the sphere be inserted in the ordered list which is normally $O(N)$, each sphere does not move far from its original location and thus will not move relatively far in the linked list. We expect the time to insert a sphere that has moved to be a constant value given that there are a constant number of spheres in the COI.

For the scenario where C_H is fixed and C_D can change, COI can degrade to $O(N)$ similar to the brute force method. The insertion operation will again become $O(N)$ as the cylinder diameter is not fixed. For extreme cases of cylinders that have height equal to the COI height then COI offers no benefit over the brute force method. In the more likely case that COI is a fraction of the cylinder height, the maximum number of calculations required are reduced by the ratio of COI search space described in Equation 57 to total cylinder area. This reduction of calculations amounts to division by a constant, so the complexity of this scenario remains at $O(N)$ regardless of collisions. If the sphere being tested will collide, then the complexity is $\Omega(1)$ and $\Omega(N)$ otherwise. Therefore, the COI method is $\Theta(c)$ for a particle movement if cylinder diameter is kept constant and $o(N)$ otherwise.

The sectoring method is a drastic improvement over COI. We developed COI due to the need to simulate electrokinetic nanoparticle (EN) treatment on larger pore sizes. For all scenarios, particle movement in sectoring is $\Theta(c)$. This is due to the fact that we must search at most eight sectors in the currently utilized implementation. Each sector

has an area described in Equation 58 that is independent of cylinder height and diameter. The search space is eight times that described in Equation 58 as eight sectors may need to be searched

$$A = (2 S_D)^3 \quad (58)$$

To summarize, COI method is efficient in regard to cylinder height increases and the sectoring method is always efficient. The search space for each method is listed in Table 4.3 for convenience. We also list for comparison the asymptotic complexities for particle movement attempts for all methods under each scenario in Table 4.4.

Table 4.3 Search space for brute force, COI and sectoring methods

Brute Force	COI	Sectoring
$\pi (C_R)^2 C_H$	$\pi (C_R)^2 (S_D + S_M + 2 B_R)$	$64 (S_D)^3$

Table 4.4 Comparison of analytical, brute force and sectoring results for 20 nm height and 50 nm diameter cylinders

	Unfixed Cylinder Diameter		Fixed Cylinder Diameter	
	Collision	No Collision	Collision	No Collision
Brute Force	$o(N)$	$\Theta(N)$	$o(N)$	$\Theta(N)$
COI	$o(N)$	$\Theta(N)$	$\Theta(c)$	$\Theta(c)$
Sectoring	$\Theta(c)$	$\Theta(c)$	$\Theta(c)$	$\Theta(c)$

CHAPTER 5

CONCLUSION AND FUTURE WORK

We present the conclusions and future work in this chapter. There are several open issues that can be addressed to continue in this area of research. We will discuss the opportunities for parallelism, alternative particle mechanics and improved user interface.

5.1 Conclusion

We have successfully created electrokinetic treatment simulation algorithms that are comparable to previous results while having lower asymptotic complexities. The sectoring method has been shown to be superior in terms of asymptotic complexity. Simulation results are similar to most physical results obtained from MIP and WLR. Some MIP results do not fall within the simulation limits, however, this is expected as MIP has been documented to be an inaccurate measure of pore distribution and porosity of concrete. Despite the disagreement between WLR and MIP, there is a trend that porosity reduction is higher 2 inches from the rebar as compared to the rebar-concrete interface. By taking the porosity reduction of cross-sectional cylindrical slices of the packed simulation cylinder, the simulation also detects a higher porosity reduction further from the rebar. The simulation indicates that this may be due to particles aggregating before reaching the rebar, and thus preventing particles from reaching the rebar. Thus

there are unfilled spaces in the cylinder that can easily be seen in the graphical representation of the simulation cylinders

We have also implemented and tested a web based framework to allow an interdisciplinary team to work in concert with access to the simulation and the results generated. The database of the framework currently holds 271 simulation runs. Simulation requests can be entered into a web interface and will automatically be processed in the order entered and the results stored into the database. Results can also be retrieved from the database and filtered based on any simulation parameter. Statistical analysis can be completed on the data points stored in the database by using version of Rweb modified by the dissertation author. The result is a collaborative framework that can be extended to address future investigations into pore packing and chloride blocking.

5.2 Parallelism

The simulation runs sequentially in the current version, that is, it only takes advantage of one central processing unit (CPU) in a given personal computer (PC). The program was also run on the PAMPA supercomputer and ran successfully, but did not take full advantage of the hardware due to the sequential nature of the algorithm. When a program is altered to take advantage of multiple processors, it is said to be threaded. Such a program is composed of threads which are separate collections of commands that can communicate and share memory. There was a test version of the simulation that had the simulation logic and graphical display on separate threads. There are additional concerns to be aware of when threading in this manner, as not all operations are "thread safe". That is, simply threading the program may lead to program crashes or other

unwanted conditions In our attempt, sometimes the program would halt temporarily until the graphical display was forced to update

On architectures such as supercomputers and clusters, memory is not shared, thus Message Passing Interface (MPI) code should be used instead As memory is not shared, messages must be passed between processing units in a much slower manner LONI and PAMPA are examples of architectures that require MPI or some similar language to take advantage of their hardware Passing messages with MPI usually requires additional overhead and performance depends heavily on the number of messages that must be sent between distinct components Compared to shared memory architectures, the message passing medium of MPI is often relatively slow Limiting the number of messages that must be passed often improves processing speed A related issue is load balancing, as each processing unit that is idle indicates an inefficiency Sometimes this inefficiency is unavoidable as the work cannot be subdivided to processors equally Processors may remain idle while waiting for messages from other processing units, thus again, limiting the number of messages that must be passed is desirable

There are many ways to parallelize a program, but we will describe a coarse grain and a fine grain implementation that may be implemented in the future Coarse grain and fine grain are not distinct methods, but rather descriptions of the method of parallelization [52] For coarse grain parallelization, problems are separated on more of a macro level For fine grain programs, problem steps are separated on more of a micro level For example, if there are students that are collaborating on solving a collection of matrix multiplication programs, they can divide the work in many different ways Assume that there are 10 such problems and two students that are collaborating If student one solves

the first five problems while student two solves the last five problems, then they are practicing coarse grain parallelization and simply concatenate the results at the end. On the other hand, if the students work on each problem simultaneously, but student one evaluates half of the resulting matrix while student two evaluates the other half, then they are practicing fine grain parallelization (or at least a finer grain). Students could parallelize at an even finer level, if for each matrix row and column multiplication necessary, student one multiplied the first half of the row while student two multiplied the last half and they sum their results to determine the value for the resulting index location.

5.2.1 Coarse Grain Parallelization

For the simulation, coarse grain parallelization simply refers to dividing the work into individual pores. If there are 10 computers and 100 pores, then each computer can be assigned 10 pores. Unfortunately, since the time required for the simulation to pack a pore varies widely depending on the conditions of the simulation as well as the performance characteristics of the computer, I suggest that a program attempt to balance the work by assigning only one pore simulation to a computer at a time. As a processing unit complete a simulation, it should report the results and be assigned another simulation if there are any remaining. Also, it may be beneficial if larger pore simulations can be given to faster computers. A proof of concept has been attempted, but due to time limitations only automatically assigns simulations to a single computer. In our solution, the target is any heterogeneous collection of computers running either Linux or Windows that have the simulation installed. Additional work is also desired to ensure that any power loss or failures in any node, including the head node, will not lead to data loss or unnecessary loss of processing time. Allocating a secondary head node similar to HA-

OSCAR or some web services may be a solution to head node failure. It will be the responsibility of the head node to assess the status of individual nodes. Given a sufficient number of requested simulations, as there is limited communication between nodes, it should be expected that the processing time will be linearly reduced by the increase in computer power. For example, if computing power is increased 10 fold, then we expect a 10 fold reduction in time. Unfortunately, this method does nothing to reduce the processing time required for an individual simulation. Also, the memory requirements for an individual simulation is not shared between computers, so multiple computers will not allow larger simulations than a single node can complete.

5.2.2 Fine Grain Parallelization

Fine grain parallelization is also desirable as it can be used to reduce the processing time needed to complete a single simulation. The author suggests that attempts at fine grain parallelization be targeted at the sectoring implementation. In this implementation, sectors should be divided between the number of processing units. I suggest that the sectors be partitioned in a manner that 1) limits the communication necessary between processing units and 2) equally distributed the work between processors. These two conditions may be slightly at odds, however, I suggest partitioning the sectors vertically. Unfortunately, each partition will share a boundary with neighboring partitions, and communication will be necessary for 1) passing a particle to another partition and 2) verifying that moving particles do not collide with particles of another partition. In a shared memory architecture, no messages need to be passed, but sectors may need to be locked to prevent race conditions. If memory is not shared, then

care must be taken to avoid deadlock and unnecessary waiting due to communication latency

Partitioning of the sectors should attempt to maintain the same number of sectors between processing units and also attempt to balance the calculation required for those sectors. This is the primary reason for choosing vertical partitions as opposed to horizontal partitions. As the sectors overlay a cylinder, it cannot simply be subdivided based on a single dimension. Instead, the cylinder boundary must be taken into account so that work can be balanced between nodes.

5.3 Particle Mechanics

Another area of potential improvement involves improving the rules that govern particle movement and collisions in the simulation.

5.3.1 Simultaneous Movement of Differently Sized Particles

In the current simulation, larger particles must be packed and fixed before smaller particles can be introduced. The COI method was chosen at first to facilitate to more easily facilitate this improvement and requires no significant change to do so. The sectoring method, on the other hand, requires a much more complex solution to model differently sized particles. As the sectoring method is much more efficient than the COI method, we will illustrate the necessary modifications. The primary issue is that when moving a larger particle around smaller particles, there are many more potential collisions to compare against. As the small spheres are contained in a smaller grid, the large sphere must check a significantly larger number of small sphere sectors. The naive approach would be to test a cubed collection of sectors that completely encapsulate the larger

sphere and its movements. However, it may be possible to test only around the boundary of the sphere using an equation similar to Bresenham's circle algorithm.

5.3.2 Additional Physical and Chemical Rules

The physical and chemical rules used to govern particle movement can be expanded. Although phenomena such as the Van Der Waals effect may not have a large area effect compared to the particle movement, it can still be taken into consideration. Also, the possibility of particles colliding and bonding together can be considered if we bound the resulting particle in a bounding sphere. The chemical binding of particles to each other or the particle wall require not only chemical equations to determine if the binding takes place, but will also require the simulation to support a narrow phase for collision detection, rotation of complex particle aggregates, as well as an improved grid management system. It may also be possible for the simulation to determine the electrophoretic velocity of each particle on the fly if enough information about the environment is available.

5.3.3 Chloride Introduction and Analysis

The simulation can simulate solvated chloride particles as 0.6 nm spheres, but that was not the focus of this dissertation. An additional grid size for these particles may be memory intensive and unnecessary. I suggest that the simulation should treat chloride ions differently in the first attempt at simulating their ingress. Given a packed particle, we can introduce a fixed number of chloride ions, say 10,000, and using the sectoring method, we can determine which sectors the chloride ions are stopped. As there are likely more than 10,000 chloride ions depending on pore size, we will be extrapolating our results. With this in mind, I suggest that interactions between solvated chloride ions

be ignored in the first attempt, or at least have this as an optional flag of the simulation. The COI method may be used effectively to manage chlorides if their introduction rate is not too high, but for 10,000 particles, even a brute force approach may be sufficient if the number of unfixed chloride particles at any given time is limited. The collision detection between the chloride ions and packed nanoparticles however should utilize the sectoring method in either case.

With these simulations, we may be able to determine a “blocking rate”, the rate at which chlorides are prevented from reaching the base of the cylinder. We can relate the blocking rate to the density of the packed cylinder, and perhaps to the composition of the packed spheres. It is not necessarily the case that the porosity of the pore is the only factor in blocking rate. We may also be able to determine the average penetration of chloride ions, as well as whether they are more likely to pass through the areas near the boundary of the cylinder rather than closer to the center of the cylinder. Furthermore, given the number of chloride ions that pass through the pore, we can determine if the rebar would rust or not at each sector based on the chloride threshold. Utilizing this information, we can determine if the packing of the given nanoparticles alone are enough to prevent chloride ingress, or if there are additional factors involved.

In some experimental results, MPI has been performed before and after EN treatment. We may be able to utilize the data collected before the EN treatment to predict the overall porosity reduction of the EN treatment given sufficient simulation runs on the appropriate pore sizes. We cannot easily predict the MPI results after the EKT treatment, as a filled pore may be detected as a distribution of smaller pores. Future research may

simulate the MPI process and determine a distribution of pore apertures that would be detected, but that is beyond the scope of this research

An alternative approach is to compare simulation results to oxidation based on chloride levels rather than porosity reduction. After a pore is packed, a number of simulated chloride ions are introduced and we attempt to move them toward the simulated rebar at the bottom of the pore. As we know the minimum concentration of chlorides needed to oxidize the rebar, we can determine if a given area of rebar is oxidized. Using the sectoring method, we need only check each sector that is adjacent to the rebar (bottom of the pore). Figure 5.1 illustrates sectors that have less chlorides than the threshold for oxidation colored as green, and those with sufficient chlorides for oxidation in red.

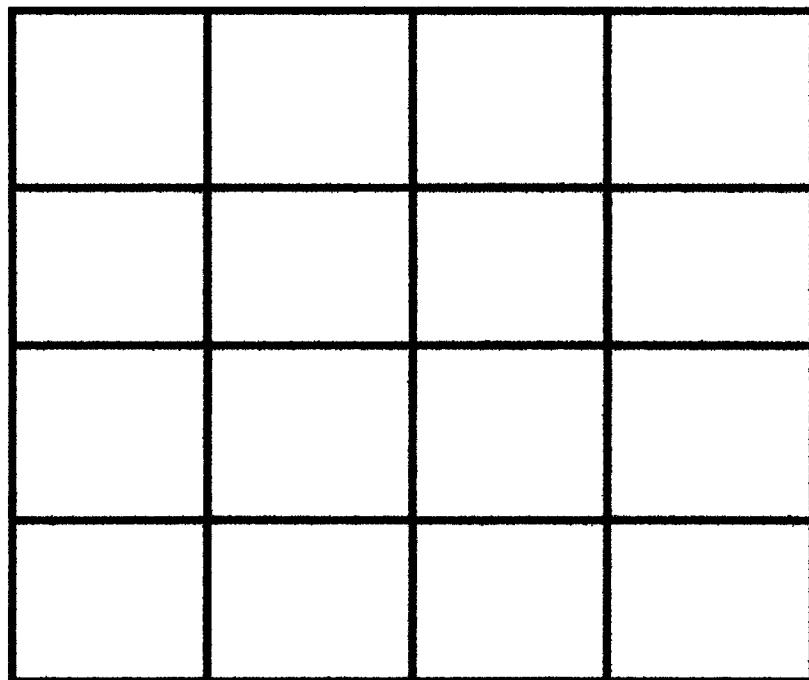


Figure 5.1 Corrosion grid

We simply count the number of each and divide the number of oxidated sectors by the number of non-oxidated sectors. In this case, there are eight oxidated sectors out of a total of 16 sectors, so we have $8/16=50\%$ of the rebar covered in rust. We again take a weighted average of oxidation based on the distribution of pores in our sample. This can be compared to the direct measurements previously collected from the rebar of physical experiments.

The simulation will have the added advantage of determining which packed pores allow chloride ingress, the percentage of chlorides blocked, and the areas of the pore that are most vulnerable to chloride ingress.

5.4 Improved User Interface

The web enabled MySQL database has served its function for this research, but it can be made more user friendly for non-computer scientists. Furthermore, it should be expanded to support coarse gain parallelization described earlier in a transparent manner. The user interface already allows multiple researchers to request multiple simulation runs, view previous results, and perform statistical analysis on results using R-web. Furthermore, it would be beneficial to save the simulated packed pore and not simply the characteristics of said pore. Although the memory requirements are larger to do so, it can save computational time if further simulation is desired on the given packed pore. For example, if we have previously packed a large pore, and now wish to determine the characteristics of chloride ingress into the pore, we can simply start from the packed pore instead of having to repack the pore each simulation. It is also desirable to have intermediate status updates on our simulations, rather than being uncertain of the

simulation progress. The programs can be adjusted to update the MySQL database at regular intervals with the number of packed pores and porosity values.

APPENDIX A

COMMAND-LINE OPTIONS

-V, --version	Gives version details Does not run program
-?, ---usage	Gives detailed usage details
-h, *//--help	
-v, --verbose	Outputs additional information during runtime
-q, --quiet	No output to command-line
-s , --sphere size=float	Adds a sphere set of a given size, you may repeat this arbitrarily for multiple sizes If none are provided, then default sphere sizes of 20 and 2nm are used in that order
-c, --concentration rate=float	Adds a concentration rate for a sphere You may repeat this up to three times The values will be applied to spheres in the same order they are entered This ,represents a percentage and should be a value from 0 0001 to 2 The upper percentage is low as particle concentrations are not high The value of course can be adjusted in source arbitrarily, but values too high become unrealistic and problematic for sphere introduction
-f, --fixed method=[off,on]	Not Yet Implemented Determines whether spheres will fix or not That is a sphere that has had limited movement options for a set amount of time will not move anymore if the fixed option is on The default is for this option to be enabled
-t, --time horizontalFixTime=integer staticFixTime=integer	The amount of time-steps that a particle will be allowed to move before it is fixed The value for horizontalFixTime refers to the number of time-steps that a particle can only move horizontally Static refers to a sphere that cannot move in any direction Vertical movement always resets sphere fixation Horizontal movement resets the staticFixTime counts

-p, --proximity	Not Yet Implemented Option to be able to have particles act differently based on the particles or cylinder boundaries nearby This would follow rules such as Van Der Waals and the algorithm would need to change to a true Monte Carlo method
-r, --random seed=integer	The seed for the random number generator If this is not supplied, zero will be used Providing a negative number will use the system time as the seed
-b, --binding method=[spheres, bottom, cylinder, all]	Not Yet Implemented Methods of spheres binding to other objects
-a, --all	Not Yet Implemented All spheres sizes are introduced simultaneously at the given rate Otherwise the default is to introduce sphere sizes one at a time from largest to smallest

Usage SectorPack [options] Diameter Height

/a out diameter height 30 20 10

APPENDIX B

MYSQL DATABASE RESULT STORAGE

Work teaching Database courses for Health Information Management improved understanding of SQL and PHP and spurred implementation of the database and web interface. After an initial testing period, final results are stored in the database starting on August 30, 2010.

For this research, a MySQL database has been created to store the results of the simulation. Requests for simulation runs can be submitted via SQL commands and are stored in the database. A script will automatically select requested simulation runs from the database and run the given simulation. Once the simulation is complete, the results are automatically added to the database.

Technical details on the creation of the database follow.

The database is named "techdata". These are the list of tables that are used "data" — requested simulations and the results (filled out later)

Explain data types and unsigned etc in ch1

cylHei unsigned int -the height of the cylinder in nm (MAX 65,535)

cylDia unsigned int -the diameter of the cylinder in nm (MAX 65,535)

poroRed float -porosity reduction

timeReq datetime -date and time the user requested the simulation

status varchar (1) - U-unassigned (default) A-assigned C-Complete

timeStart datetime -date and time simulation actually started

timeEnd datetime -date and time simulation completed

numPart int -how many different particle sizes (Max 3, assumed 2)

part1 float -first particle size (assumed 20)

part2 float	-second particle size (assumed 2)
part3 float	-third particle size (assumed NULL)
seed int	-initialized the random number generator (Default 0)
p1Num int	-number of particles of size 1
p2Num int	-number of particles of size 2
p3Num int	-number of particles of size 3

COMMANDS to create appropriate MySQL tables (password should be replaced with the password)

create database techdata,

grant SELECT, INSERT ON techdata * TO Web@'localhost' IDENTIFIED BY 'password',

create table data(PID int Auto_Increment, cylHei smallint unsigned, cylDia smallint unsigned, poroRed float, timeReq datetime, status varchar(1) DEFAULT 'U', timeStart datetime DEFAULT NULL, timeEnd datetime DEFAULT NULL, numPart int DEFAULT 2, part1 float DEFAULT 20, part2 float DEFAULT 2, part3 float DEFAULT NULL, seed smallint unsigned DEFAULT 0, p1Num bigint, p2Num bigint, p3Num bigint, Primary Key(PID)),

APPENDIX C

SIMULATION WEB INTERFACE

There is a web interface for the simulation, currently at <http://138.47.32.82/Electroschedule/stats.php>. The web interface is an alternative to running the simulation application on either a Windows or Linux based computer. The web interface is a simple GUI-based interface that remotely runs the Linux version of the application. Linux was chosen as the target as it is the more common operating system for parallel computing systems such as PAMPA, LONI and Beowulf clusters.

A web interface has several advantages over running the application manually:

- 1) The web interface can be used by many devices IBM-compatible computers (Windows and Linux), Macintoshes, smart phones, and gaming systems (PlayStation 3 and Wii) and is consistent among all devices.
- 2) The application speed is independent of the user's computer. As the application runs on a remote computer, there is no performance loss on the user's computer. Even old computers or relatively low speed devices such as cell phones can use the web interface with no loss of simulation performance.
- 3) The application runs independently of the user's computer. A user may queue results and close the web page or even shut down their computer without affecting the results. The user may simply revisit the web interface at a later time to check the progress of their simulation query and view the results if it has completed. Remote access using putty will end a simulation if the connection is interrupted, but not with the web interface.
- 4) The web interface is a simple web page and requires very little technical skill to utilize. The user does not have to compile the source code for their particular

system. The user does not need to understand command line options, sequential query language or how to create batch files to run the program.

- 5) The web interface encapsulates the simulation and many changes to the simulation require no special action from the user. Thus the simulation can be updated without affecting the web interface. The web interface can also be updated in conjunction with the simulation, but this requires no special action by the user.
- 6) Results obtained by one user are available to all other users. All results are compiled in a single place that is query-able with SQL, but appear to the users as checkboxes and drop-down list.

The web interface also has some limitations compared to the application:

- 1) No intermediate output, that is, there will be no feedback until the simulation is complete.
- 2) The graphical version of the simulation cannot be run through the web interface, only the results are presented.
- 3) An internet connection is required to use the web interface. A Web browser is also required.

There are several pages available through the web interface that can give a variety of information as the user requires it. At the top of each page is a menu that contains links to status, sources, requests and results.

On the status page shown in Figure C-1, the overall status of simulations is displayed. Jobs are either assigned, completed or unassigned. An assigned job is

currently undergoing processing A completed job has already been processed and the results are stored in the database Unassigned jobs have not been processed, and are awaiting an available computer to be processed

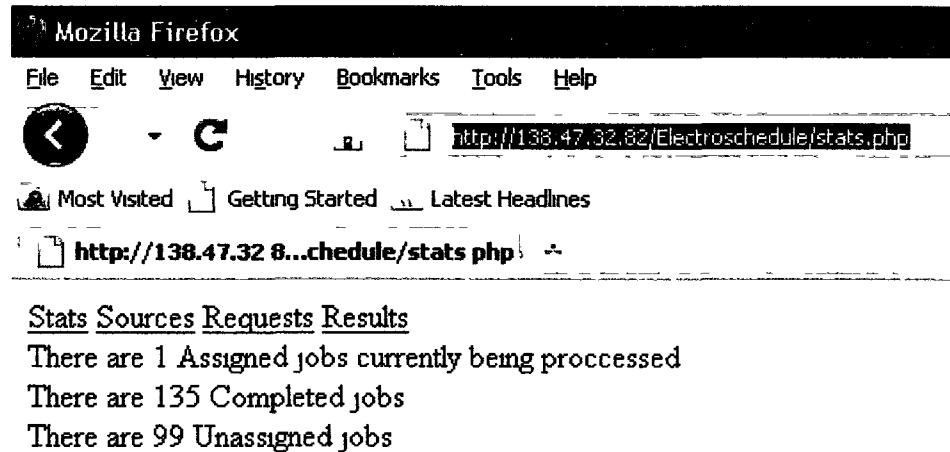


Figure C-1 Web interface status screen

The sources page is planned to include a list of all computers by IP address or URL, as well as the machine details You will be able to add new computers and verify their legitimacy The intent is for this page to facilitate coarse grain parallelization in the future

The requests page is used to request a new simulation run as shown in Figure C-2 You are required to enter a cylinder height and diameter in nanometers The default for both is 20 nm You must also have at least one particle size chosen, but you may enter three at most The sizes should be entered largest first, Thus the value entered for “diameter 1” should be greater than the value entered for “diameter 2” which is in turn greater than the value entered for “diameter 3” The default values are 20 nm for the

larger sphere size and 2nm for the smaller sphere size. Below, you must select to either run a single run or multiple runs with the given values. Each simulation run results vary based on a seed for a random number generator. If multiple runs are chosen, then the random seed will be chosen to be different from all previous results. If a single run is chosen, the user will be asked to enter a random seed. The user can verify that simulation runs with the same seed yield the same results with this option. If the user wants a single run with a guaranteed unique seed, they may choose multiple runs and set the number of runs to one. The entry forms described can be seen in Figure C-2.

The screenshot shows a Mozilla Firefox browser window. The title bar says "Mozilla Firefox". The menu bar includes "File", "Edit", "View", "History", "Bookmarks", "Tools", and "Help". The toolbar has icons for back, forward, search, and home. The address bar shows the URL "http://138.47.32.82/Electroschedule/request.php". Below the address bar, there are links for "Most Visited", "Getting Started", and "Latest Headlines". A new tab button is visible. The main content area displays a form for simulation requests. It has sections for "Cylinder" and "Particles". Under "Cylinder", there are fields for "Height" (20) and "Diameter" (20). Under "Particles", there are fields for "Diameter 1" (20), "Diameter 2" (2), and "Diameter 3" (empty). At the bottom, there are radio buttons for "Single Run" and "Multiple Runs", and a "Submit Query" button.

Figure C-2 Web interface simulation request screen

Figure C-3 Web interface single and multiple simulation entry forms

When the submit query button is clicked, the request will be queued To enter similar requests quickly, click the back button on the browser instead of using the menu The results section is used to retrieve results If the submit button is clicked using the default values, all the results will be displayed This includes results that have not yet completed Incomplete information will instead display NULL instead of a numeric value

The Porosity reduction Options are used to view aggregated results for porosity over cylinder diameter, height, or both diameter and height The user may choose to view any combination of average porosity, maximum porosity, or minimum porosity The user may also choose what fields to display by clicking the checkboxes under fields to display shown in Figure C-4 and Figure C-5

No constraints

PID	=	<input type="button" value="Add Constraint"/>
Porosity Reduction Options		
<input type="checkbox"/> Average <input type="checkbox"/> Minimum <input type="checkbox"/> Maximum		
Grouped by		
Diameter	Height	
Fields to Display		
<input checked="" type="checkbox"/> Cylinder Diameter <input checked="" type="checkbox"/> Cylinder Height <input checked="" type="checkbox"/> Porosity Reduction <input checked="" type="checkbox"/> Particle 1 Diameter <input checked="" type="checkbox"/> Particle 2 Diameter <input type="checkbox"/> Particle 3 Diameter <input checked="" type="checkbox"/> Particle 1 Quantity <input checked="" type="checkbox"/> Particle 2 Quantity <input type="checkbox"/> Particle 3 Quantity <input type="checkbox"/> Time Simulation Requested <input type="checkbox"/> Time Simulation Started <input type="checkbox"/> Time Simulation completed <input type="checkbox"/> Number of particle sizes <input type="checkbox"/> Status <input type="checkbox"/> Seed for Random Numbers		
<input type="button" value="Submit"/>		

Figure C-4 Web interface result request screen

No constraints

PID	=	<input type="button" value="Add Constraint"/>
Porosity Options		
cylHei	<	<input type="checkbox"/> Minimum <input type="checkbox"/> Maximum
cylDia	>	
poroRed	y	
timeReq	er	
status	Height	
timeStart		
timeEnd		
numPart		
part1	Diameter	<input checked="" type="checkbox"/> Cylinder Height
part2	1 Diameter	<input checked="" type="checkbox"/> Particle 2 Diameter
part3	1 Quantity	<input checked="" type="checkbox"/> Particle 2 Quantity
seed	ulation Requested	<input type="checkbox"/> Time Simulation Started
p1Num		
p2Num		
p3Num	Number of particle sizes	<input type="checkbox"/> Status

Figure C-5 Web interface result request dropdown box

The drop-down lists at the top are used to retrieve records with certain characteristics. Each constraint must be added one at a time by filling in the values and clicking the add constraint button. For example, the user might only want simulation results where the larger particle size is 20 nm and the smaller particle size is 2 nm as shown in Figure C-6.

part1='20' AND part2='2'

part2	=	2	Add Constraint
-------	---	---	----------------

Figure C-6 Web interface where clause entry

After the user has selected the options they desire, they can click the submit button at the bottom of the web page to view the results of their query. The results will be presented in a table with the fields listed in the first row as shown in Figure C-7.

Stats Sources Requests Results

cylDia	cylHei	poroRed	part1	part2	p1Num	p2Num
1000	100	0.590052	20	2	8704	2359475
50	20	0.650133	20	2	4	2095
50	20	0.582293	20	2	2	3459
50	20	0.620267	20	2	3	2815
50	20	0.616747	20	2	3	2782
50	20	0.582187	20	2	2	3458
50	20	0.612693	20	2	3	2744
50	20	0.618667	20	2	3	2800
50	20	0.609493	20	2	3	2714
50	20	0.612907	20	2	3	2746
50	20	0.620907	20	2	3	2821
100	100	NULL	20	2	NULL	NULL
100	100	NULL	20	2	NULL	NULL
100	100	NULL	20	2	NULL	NULL

Figure C-7 Web interface results output

APPENDIX D

COMPILED INSTRUCTIONS

The COI and Sectoring based simulation is compiled using gcc MingW can be used instead for Windows based operating systems with minor modifications to the source code In particular, only the Windows version of the program supports the graphical display Linux would also be capable of a graphical display, but the Timer class used to maintain the frame rate is Windows dependent, so would need to be rewritten to support graphics in Linux A windows version was also threaded at one point, but threading is platform dependent as well The files necessary for the non-graphical sectoring version are

Sphere.cpp

SphereCylinder.cpp

Sector.cpp

SpherePacking.cpp

and can be compiled by

```
g++ -o test.exe SpherePacking.cpp
```

Additionally, the graphical version of the program requires

Timer.cpp

freeglut.dll

and can be compiled in Windows by

```
g++ -o test.exe SpherePacking.cpp -lfreeglut -lopengl32 -lglu32 -lwinmm
```

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